



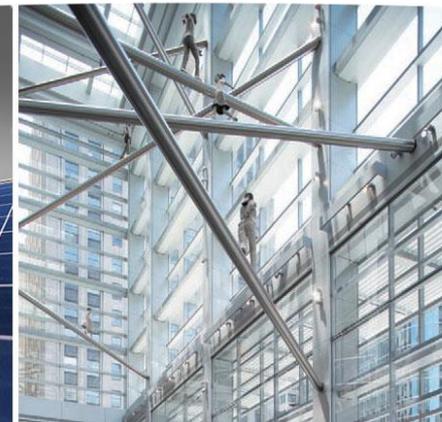
**PPG Flat Glass**

Bringing innovation to the surface.™

# Flat Glass Production Using the Float Process

Gerald DiGiampaolo and Rajiv Tiwary  
Contributions by Chuck Edge

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# Presentation Outline

Float Process History

Process Tour

- Glass Delivery System

- The Float Bath

- The Bath Exit

The Equilibrium Thickness Concept

Ribbon Forming

Optical Distortion

Heat Transfer

Bath Chemistry

Bath Modeling

# Float Process History

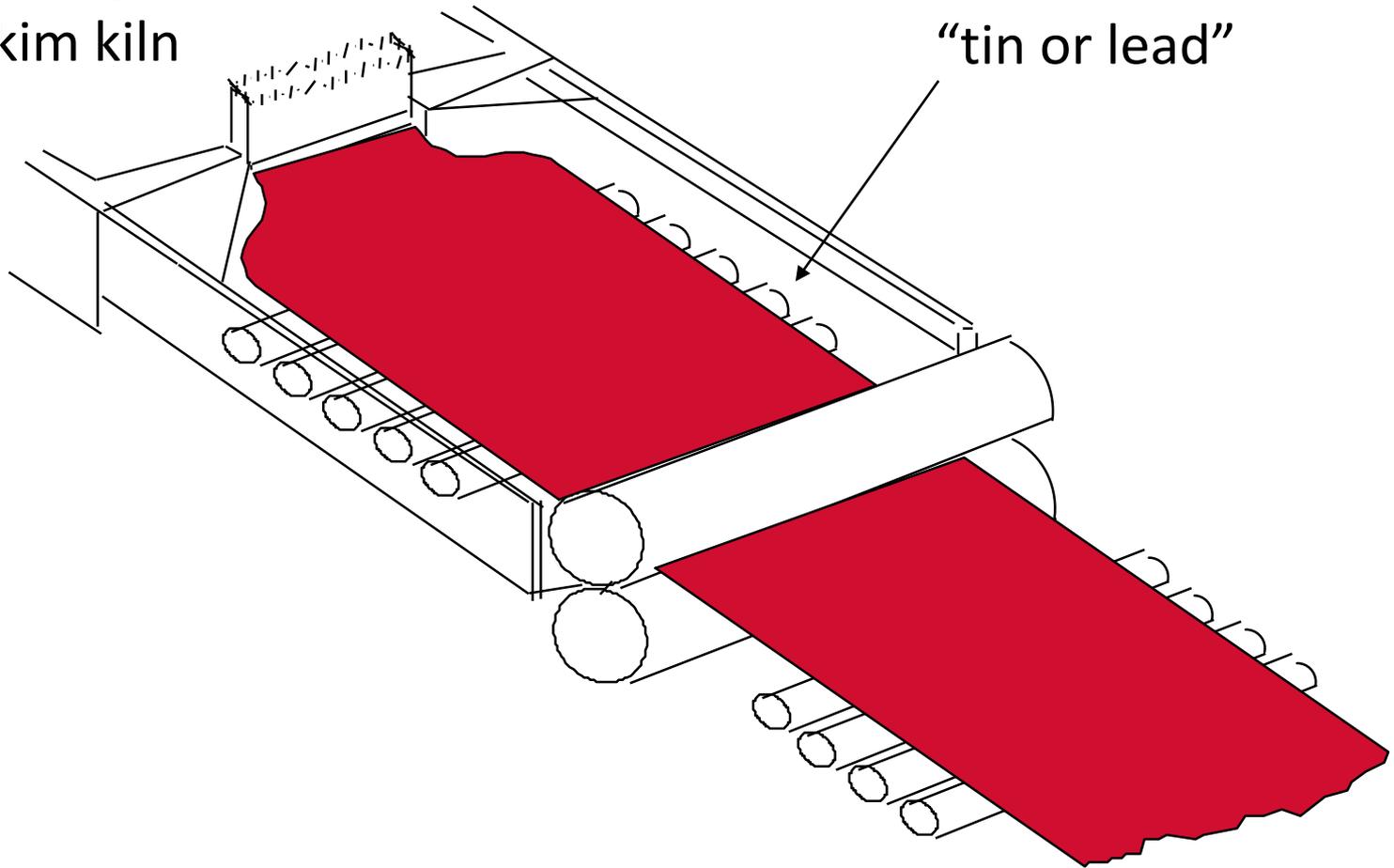
# Float Glass Manufacture (A Brief Patent History)

<b>Inventor</b>	<b>Year</b>	<b>Comments</b>
Bessemer (Brit.)	1848	annealer, fire-polisher
Lombardi (Ital.)	1900	capacitors
Heal	1902	first "float glass" patent
Hitchcock	1905	direct stretch concept
Heal	1925	melt directly on tin
Hitchcock	1928	unhindered lateral flow
Pilkington	1965	first Pilkington patent (U. S.)
Edge et. al.	1974	PPG process

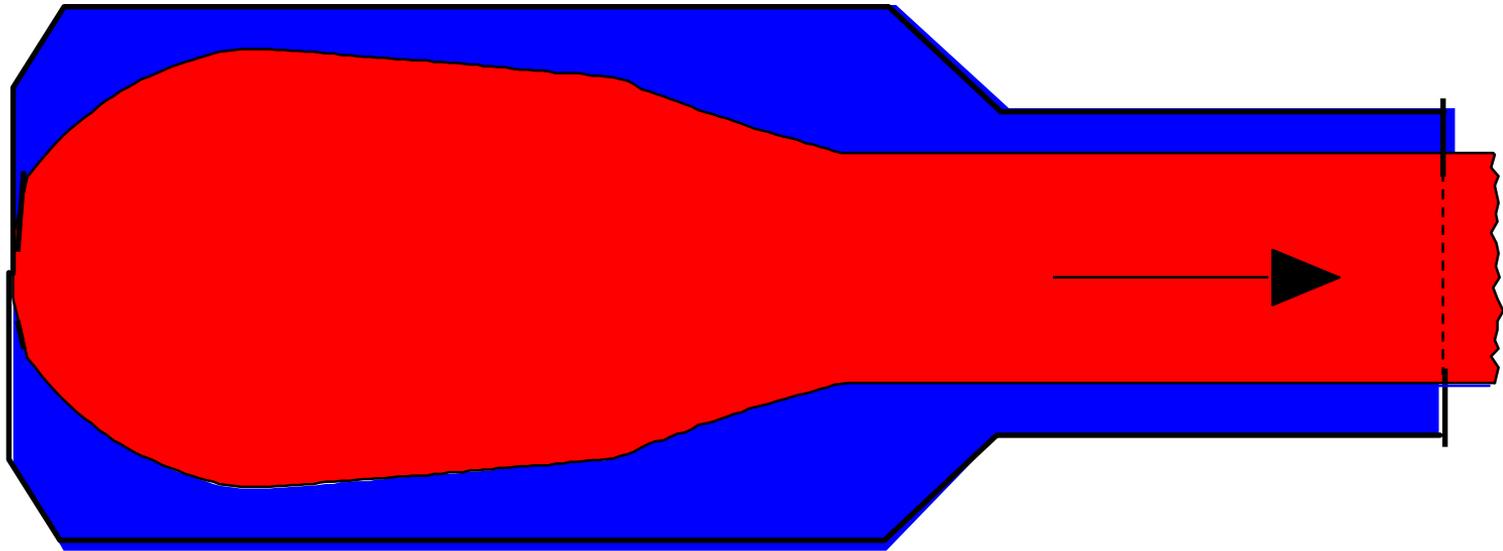
# An Early “Float” Concept

plate glass  
skim kiln

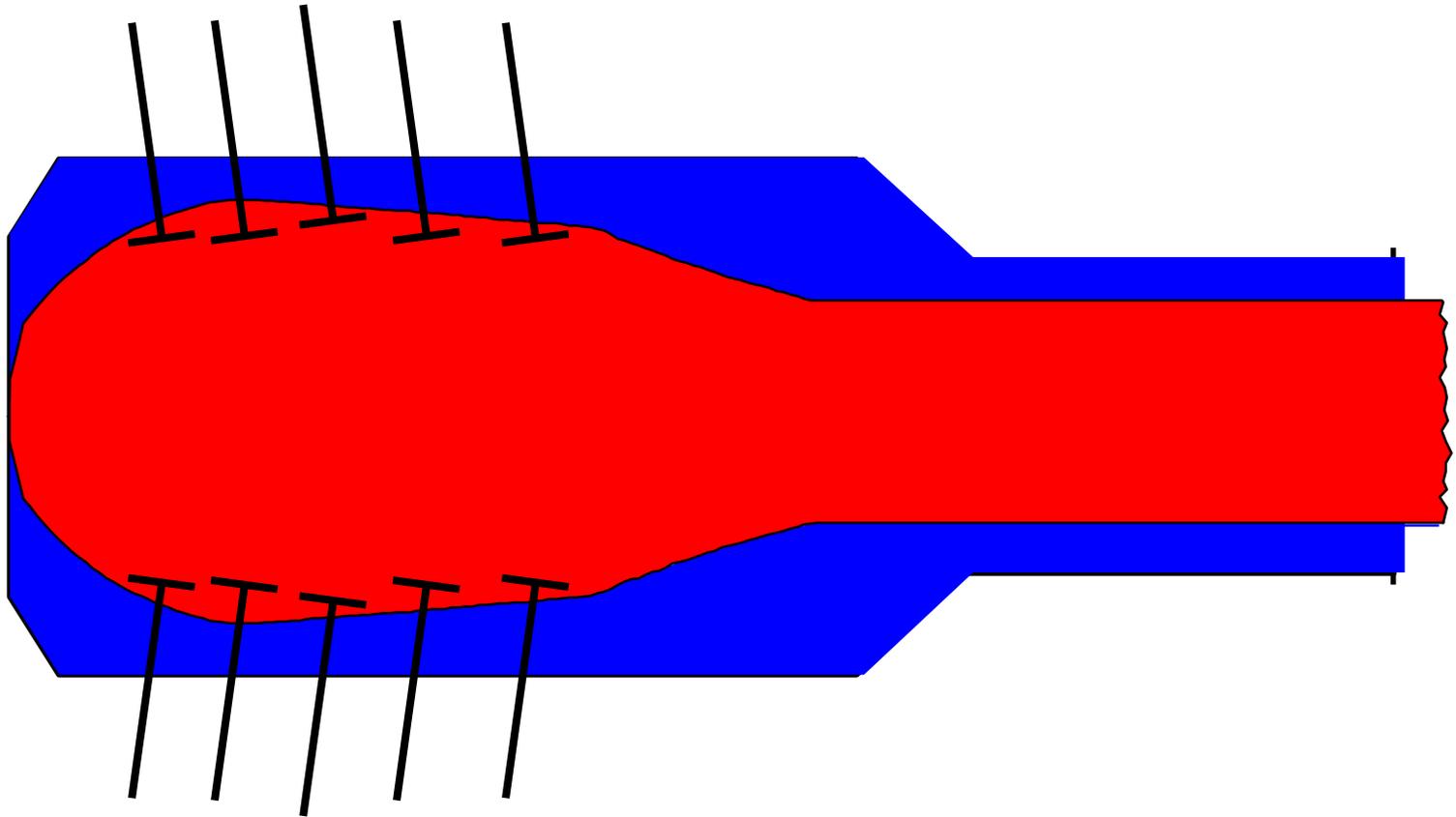
“tin or lead”



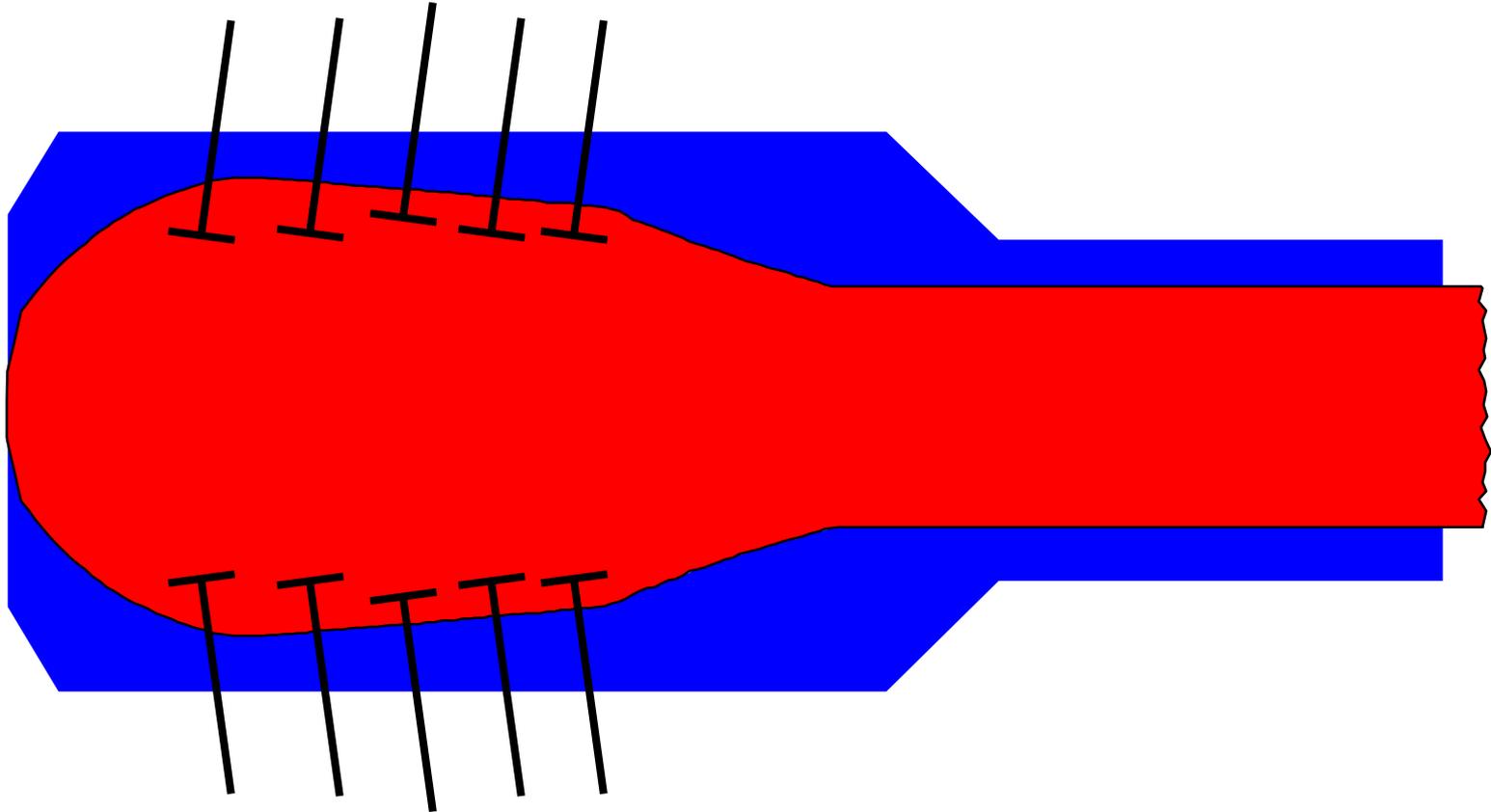
# The Direct Stretch Process



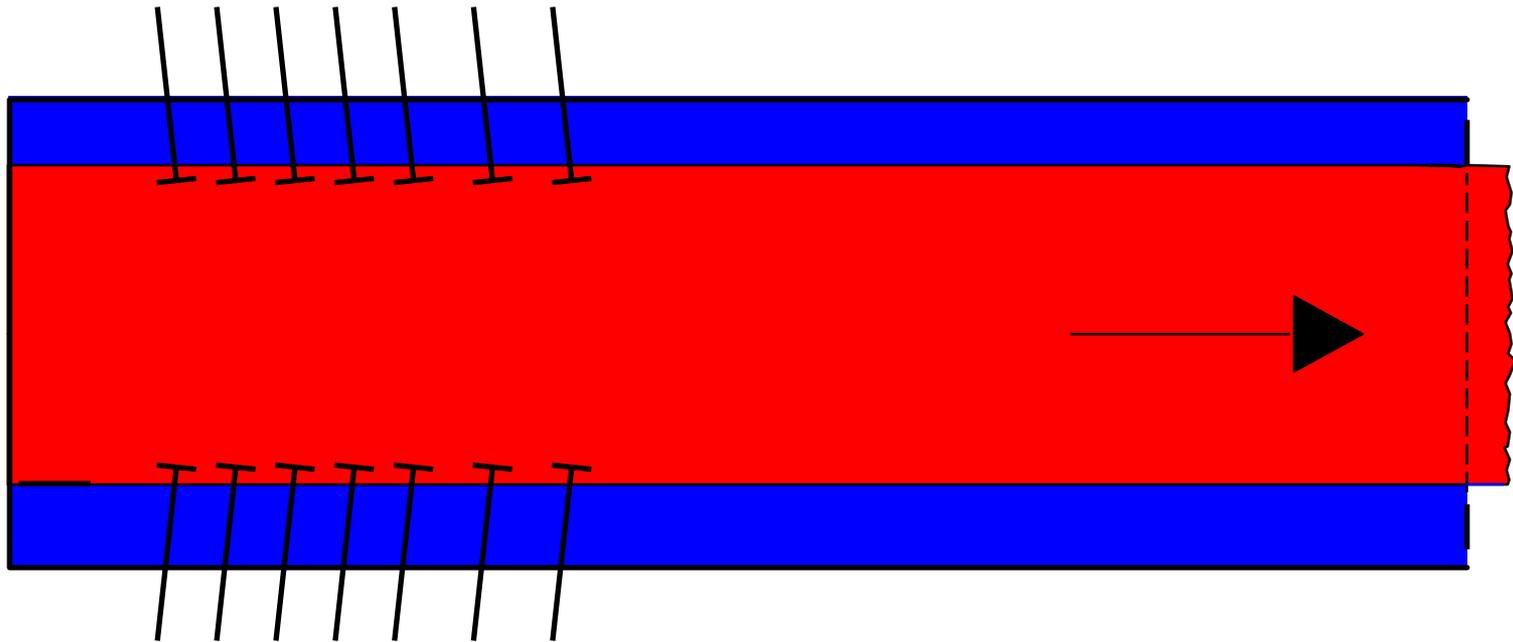
# The Assisted Direct Stretch (ADS) Process *(to produce glass <equilibrium thickness)*



# The Reverse Assisted Direct Stretch (RADS) Process (to produce glass $\geq$ equilibrium thickness)

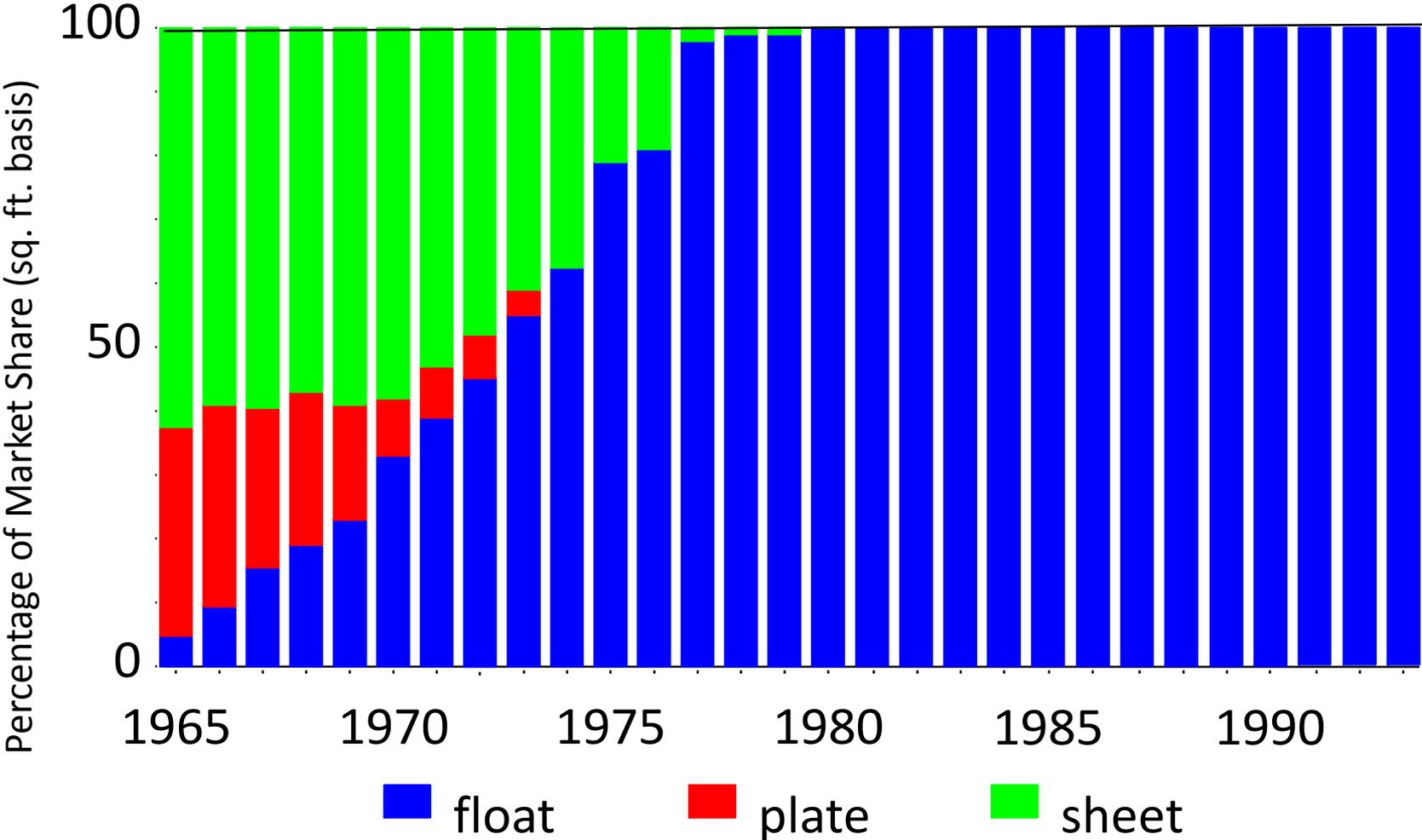


# The PPG Process



# Primary Glass Processes

## U. S. Market Share



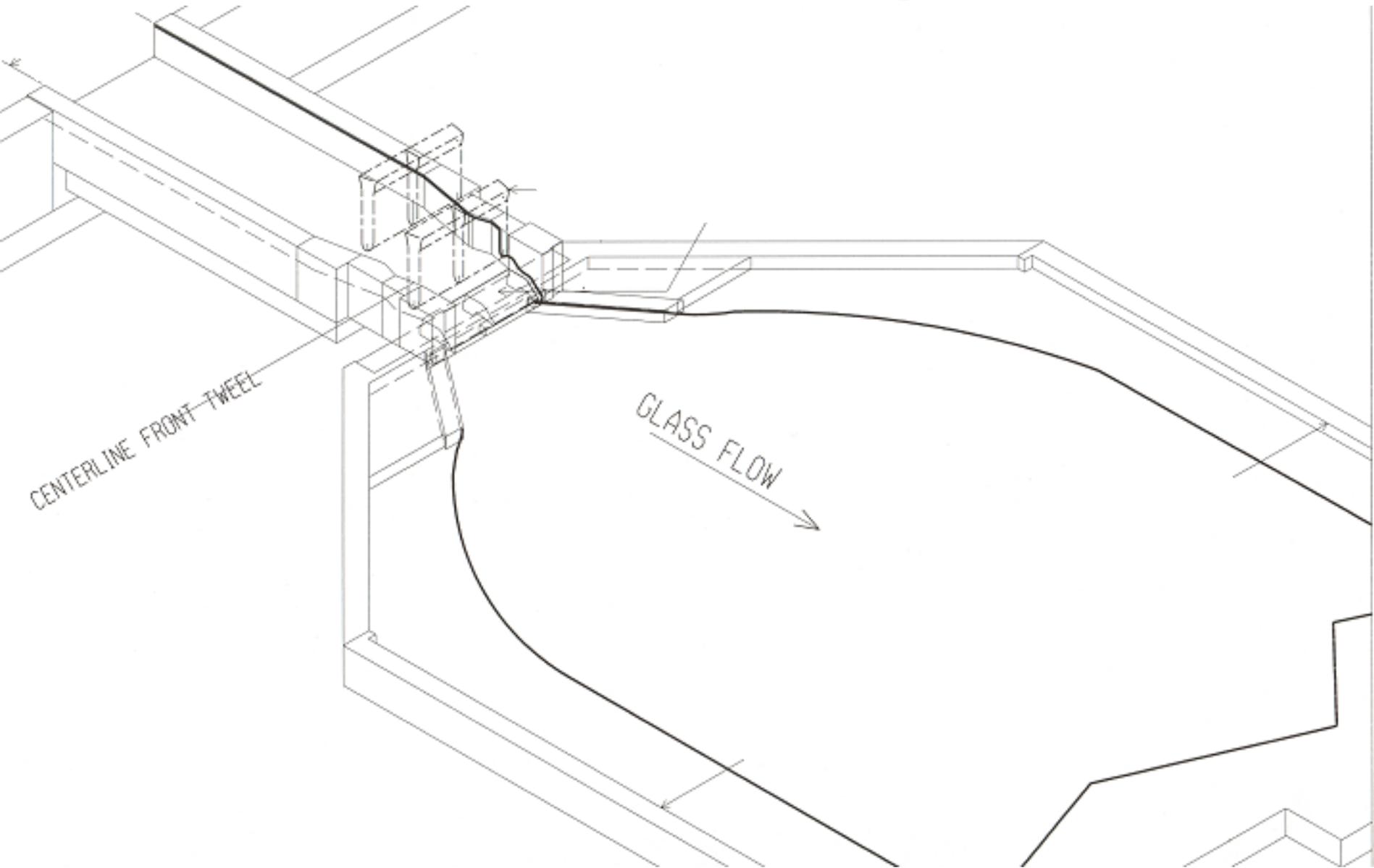
# Process Tour

# Functions of a Float Bath

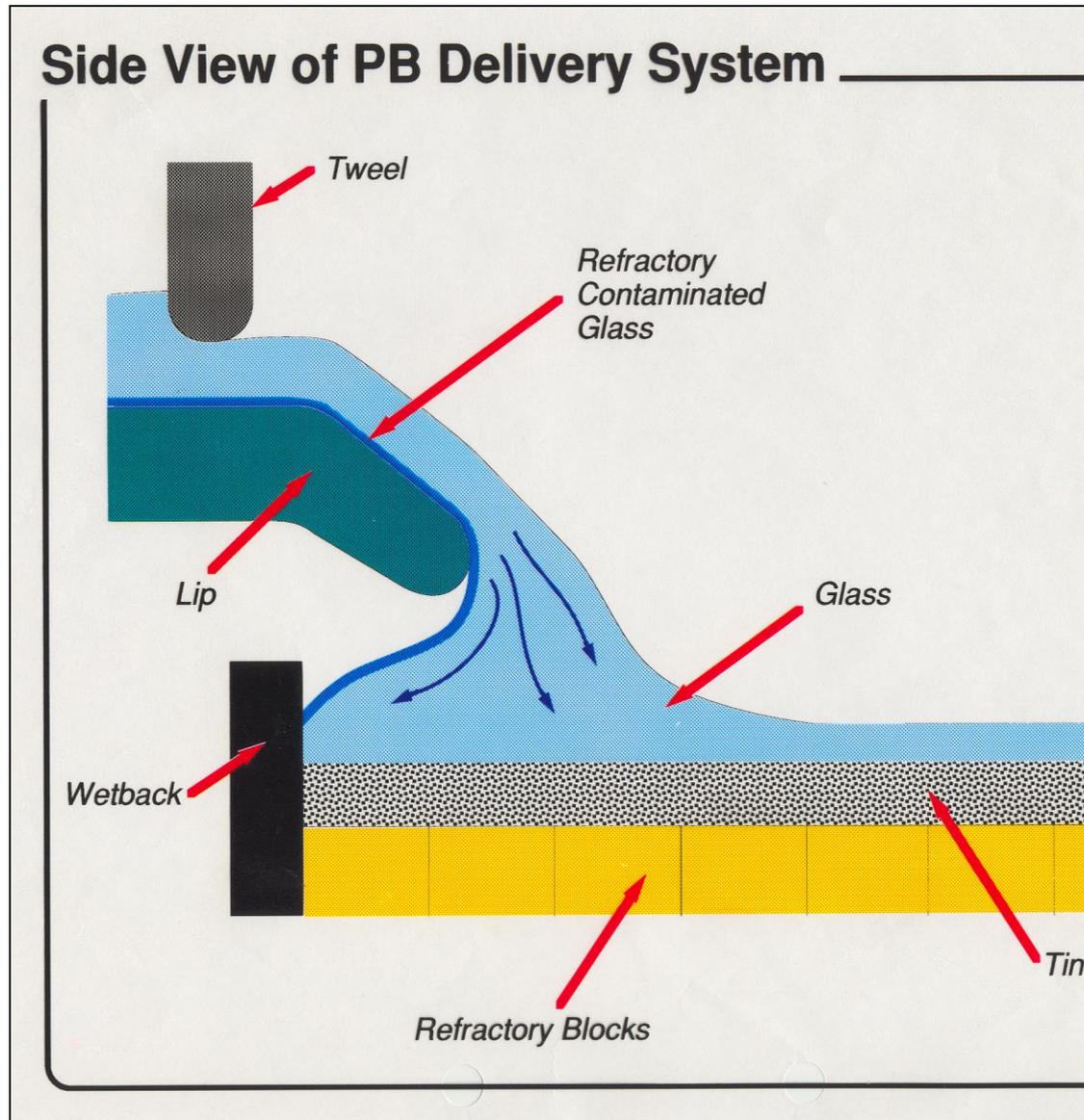
- Need to produce glass as flat as possible
  - Bottom surface becomes flat since liquid tin (very dense) provides flat surface
  - Top surface becomes flat by glass flow due to gravity
- Need to produce glass to needed thickness and width
  - ADS machines are used
- Need to cool glass from 1100 C to 600 C
  - Coolers are used at appropriate locations
- Tin must not get oxidized
  - Bath atmosphere kept reducing 95% N<sub>2</sub> + 5% H<sub>2</sub>

# Glass Delivery to the Tin Bath

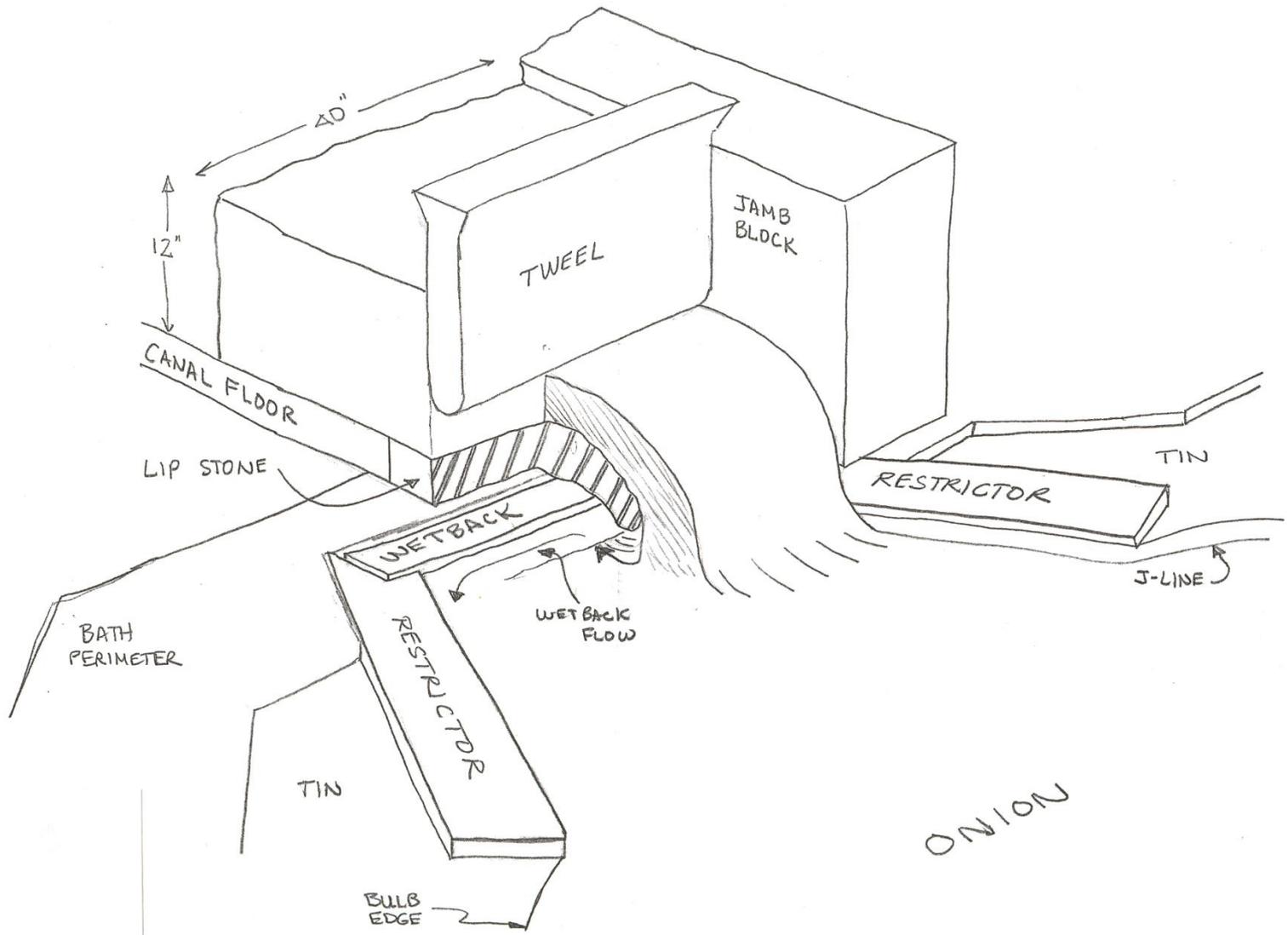
# Glass Delivery



# Glass Delivery System

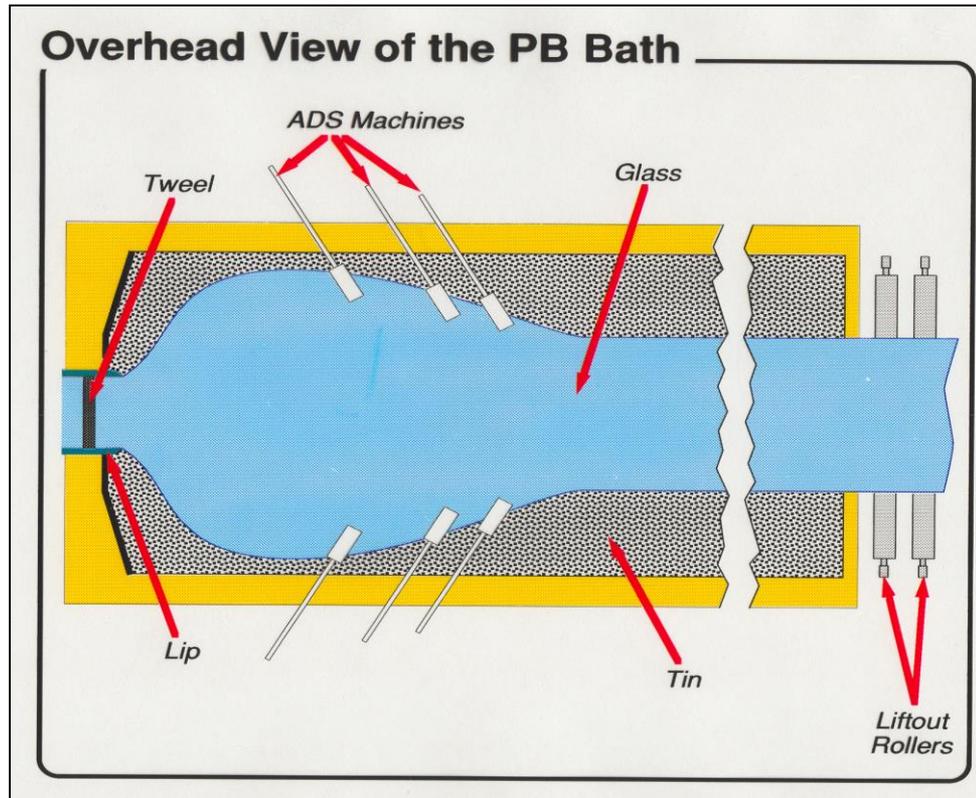


# Glass Delivery System



# The Float Bath

# Overhead View of Ribbon on Tin

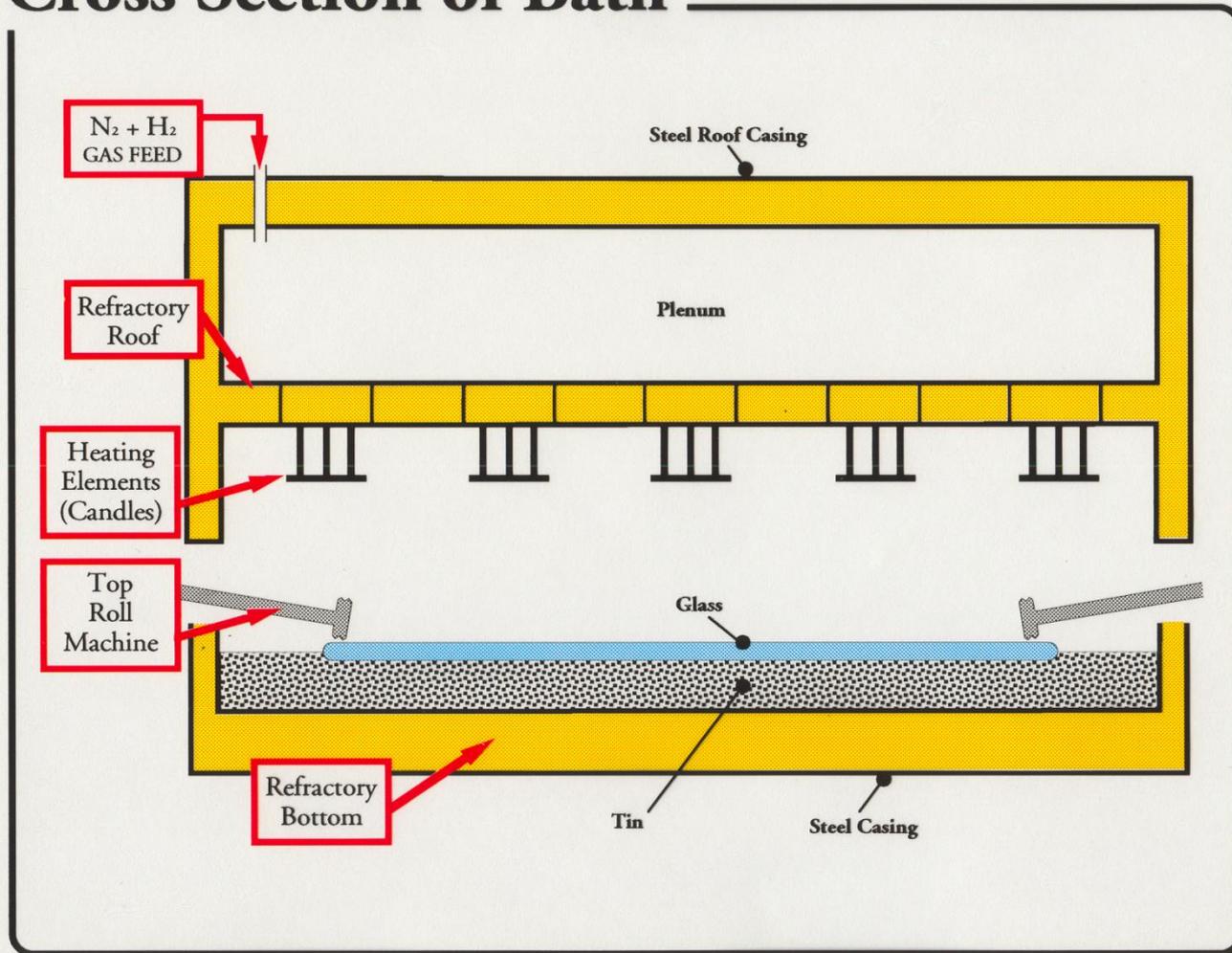


Glass flows onto the tin at a thickness of approximately 5 cm and spreads to achieve an equilibrium thickness of .6909 cm.

The lehr force is attenuating the glass to a final thickness less than equilibrium. The internal stress in the glass attempts to narrow the ribbon back to equilibrium thickness. The outward force imposed by the ADS machines minimizes the collapse to produce a ribbon of desired thickness and width.

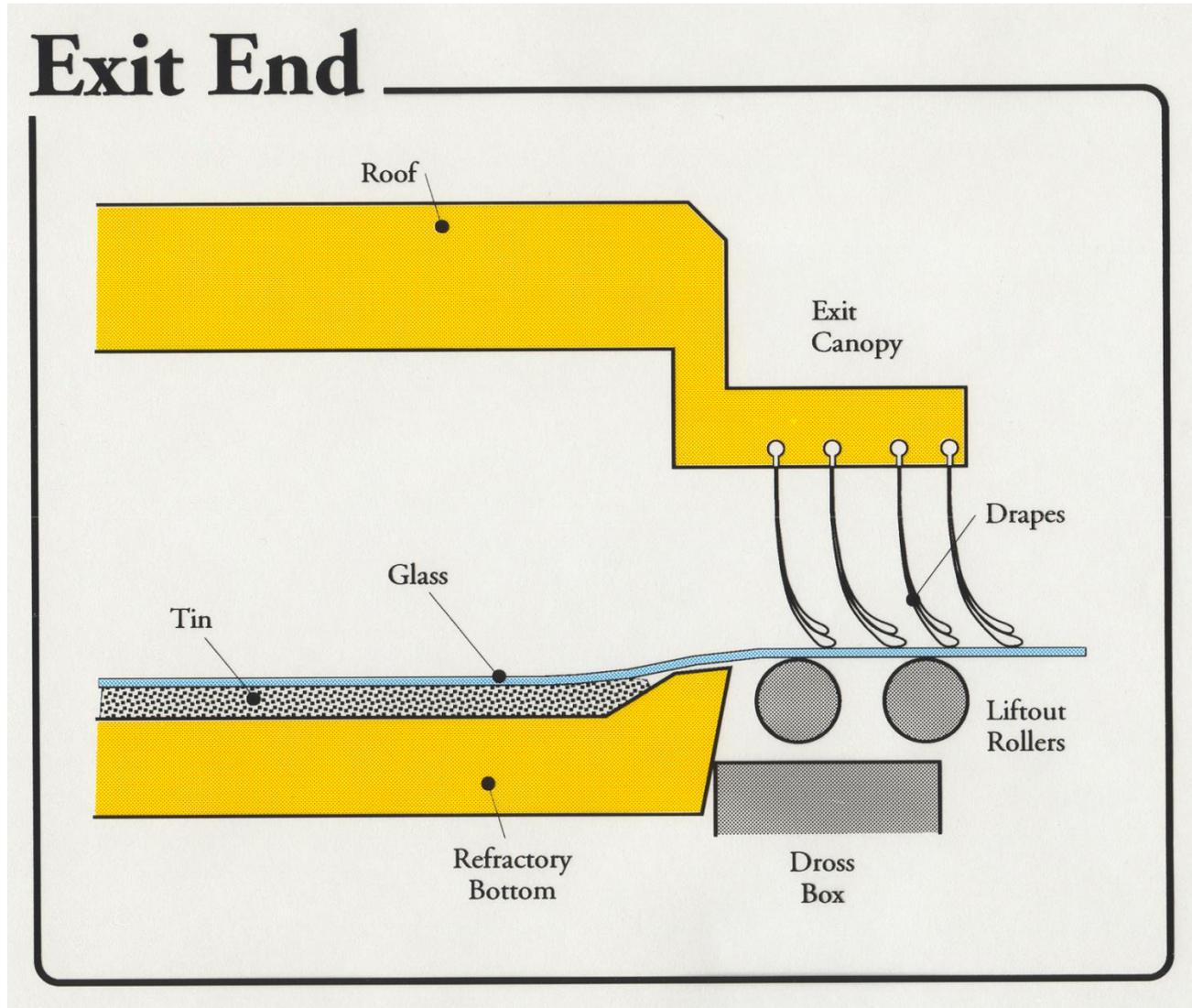
# Float Bath Cross Section

## Cross Section of Bath



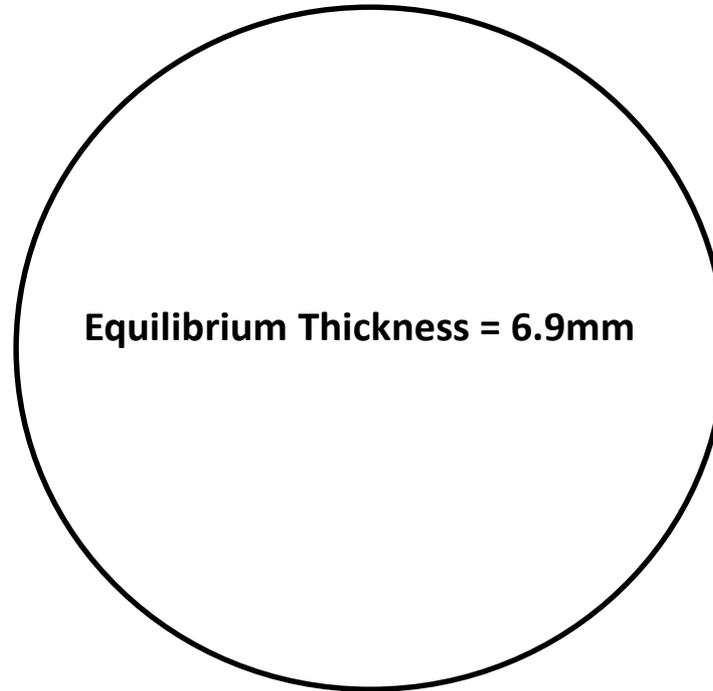
# The Bath Exit

# Ribbon Removal from Float Bath



# Equilibrium Thickness

# Equilibrium Thickness



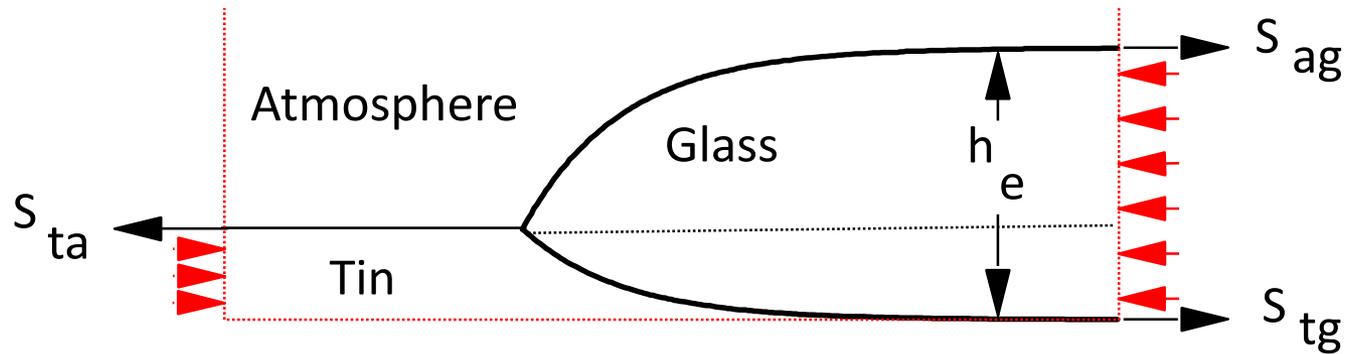
When molten glass is poured onto tin, it will spread until the interfacial tensions and gravitational forces are balanced, resulting in a circular glass-tin interfacial shape with an equilibrium thickness of 6.9mm.

When forming a continuous ribbon, the glass will always attempt to achieve equilibrium thickness.

If the glass thickness is less than 6.9mm, the ribbon will collapse to become thicker.

If the glass thickness is greater than 6.9mm, the ribbon will spread to become thinner.

# Equilibrium Thickness - A Free Body Diagram



**Equilibrium Thickness = 6.9mm**

$$h_{eq}^2 = \left( S_{tg} + S_{ag} - S_{ta} \right) \frac{2\rho_t}{g\rho_g (\rho_t - \rho_g)}$$

# Some Material Properties

## Density

glass  
tin

2400 kg/m<sup>3</sup>  
6500 kg/m<sup>3</sup>

## Surface Tension

glass/air  
glass/tin  
tin/air

.318 N/m  
.528 N/m  
.497 N/m

## Viscosity

glass  
tin

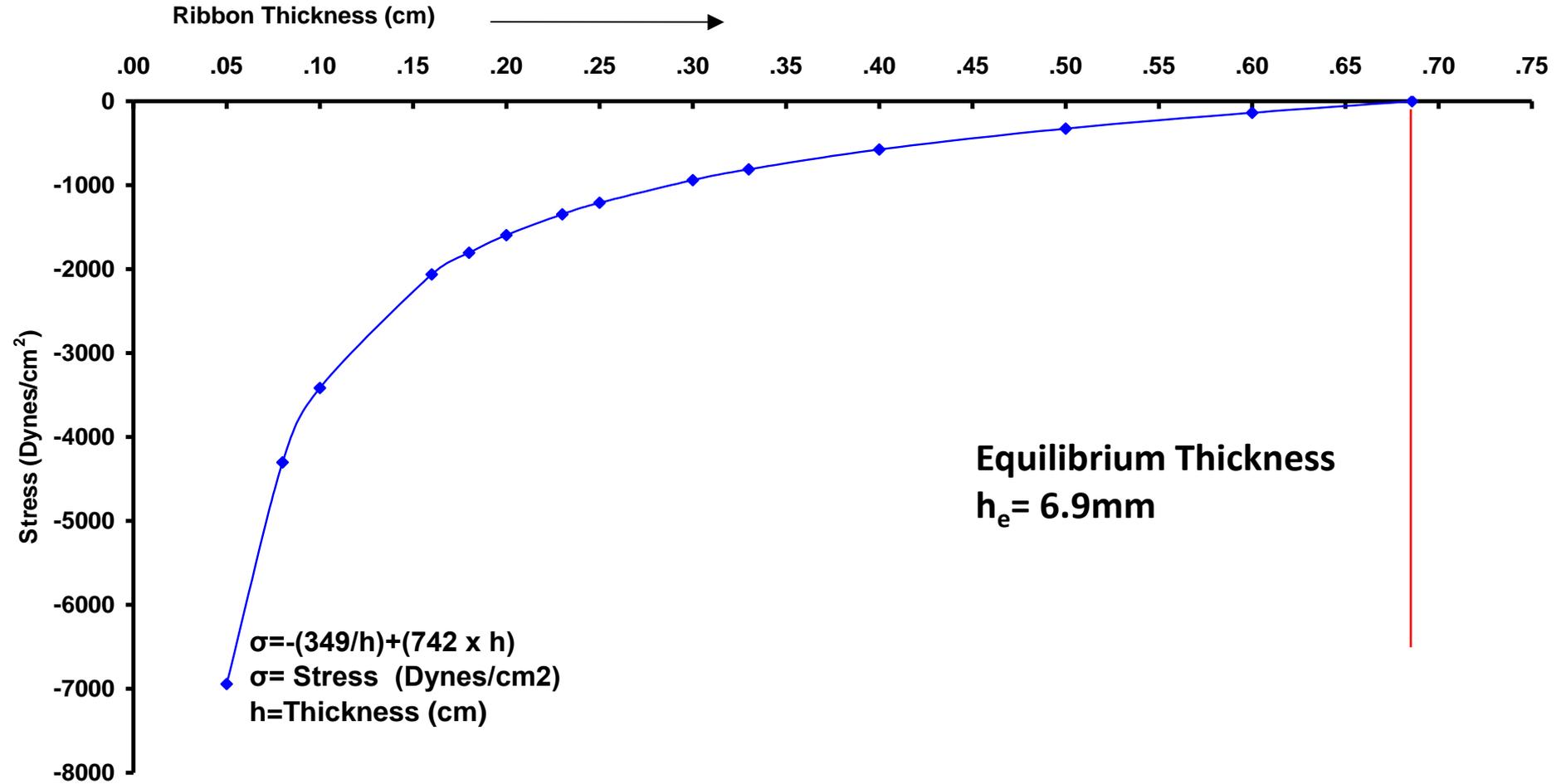
10<sup>2</sup> to 10<sup>9</sup> Pa-s  
.001 Pa-s

## Thermal Conductivity

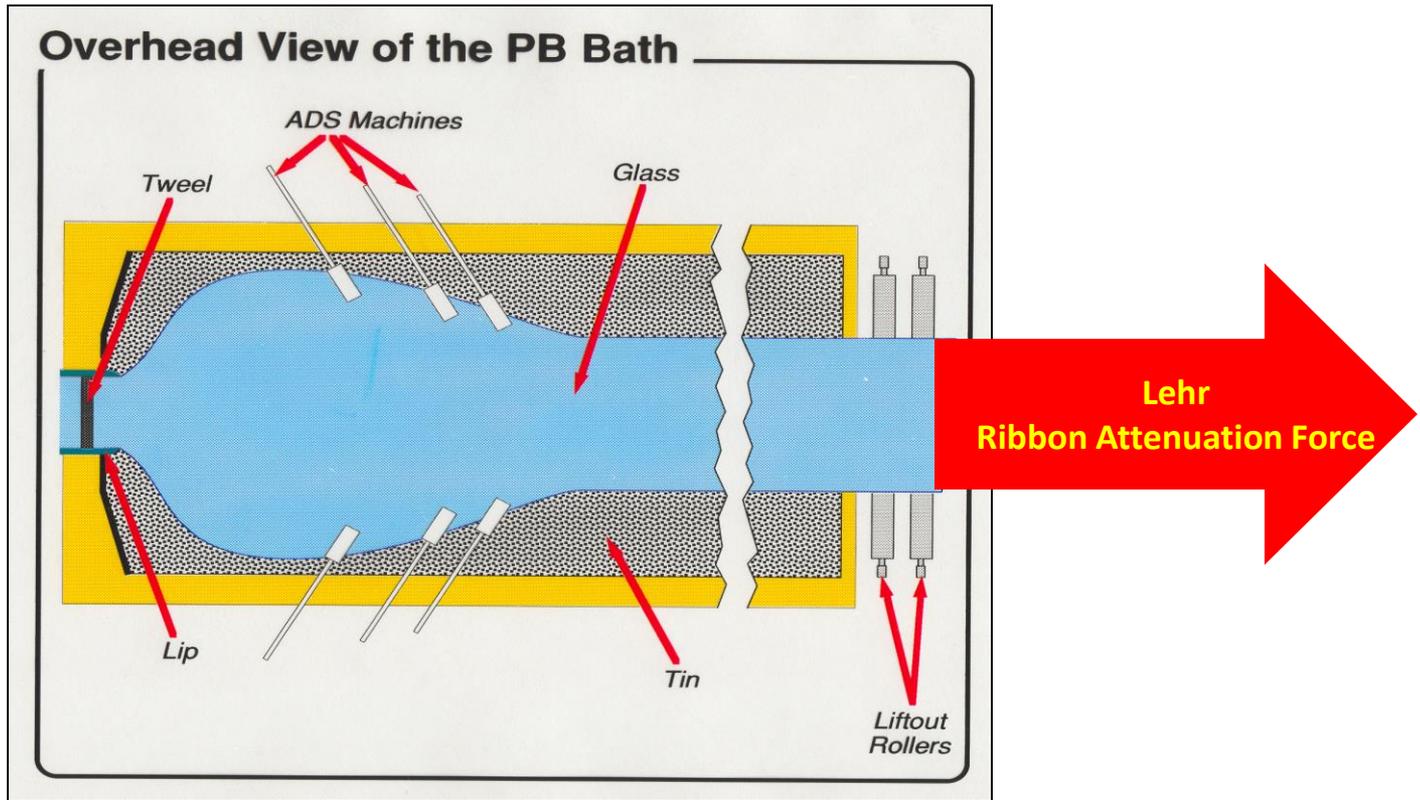
glass  
tin  
fused silica  
Walsh 71 refractory

1 W/m-K  
46 W/m-K  
1 W/m-K  
2 W/m-K

# Ribbon Stress vs Thickness



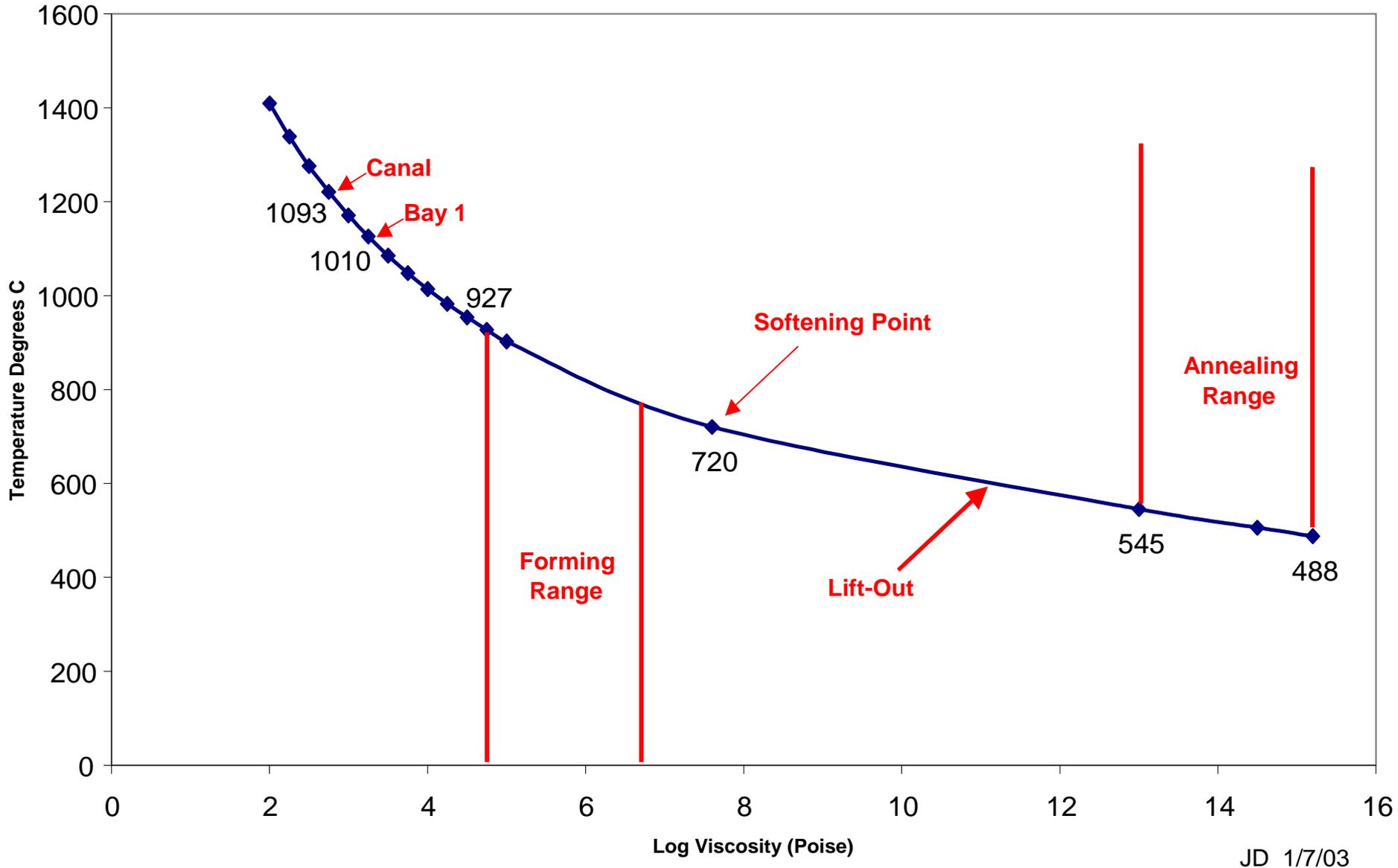
# Ribbon Forming



Glass flows onto the tin at a thickness of approximately 5 cm and spreads to achieve an equilibrium thickness of .6858 cm.

The lehr force is attenuating the glass to a final thickness less than equilibrium. The internal stress in the glass attempts to narrow the ribbon back to equilibrium thickness. The outward force imposed by the ADS machines minimizes the collapse to produce a ribbon of desired thickness and width.

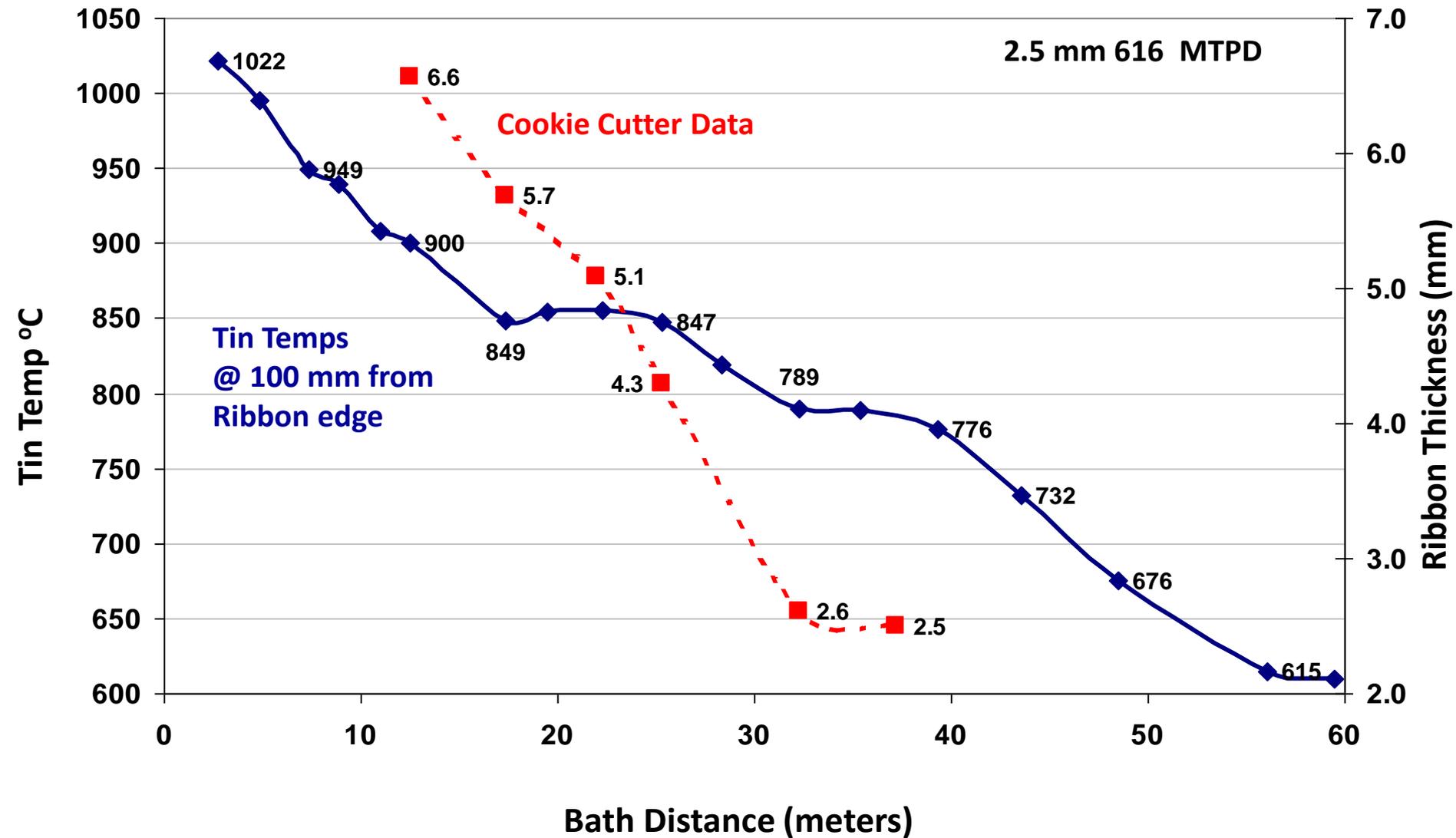
# Viscosity vs Temperature



# Forces: An Example Using a Typical Float Bath Setup

Force	First Machine (dynes)	Last Machine (dynes)
Inertia	0.04	0.47
Hydrostatic	590	317
Surface Tension	-590	-750
Net	0	-433
Tin Friction (bottom surface)	5.5	113
Longitudinal Lehr Force (ribbon attenuation)	161	5279

# Tin Temperature and Ribbon Thickness

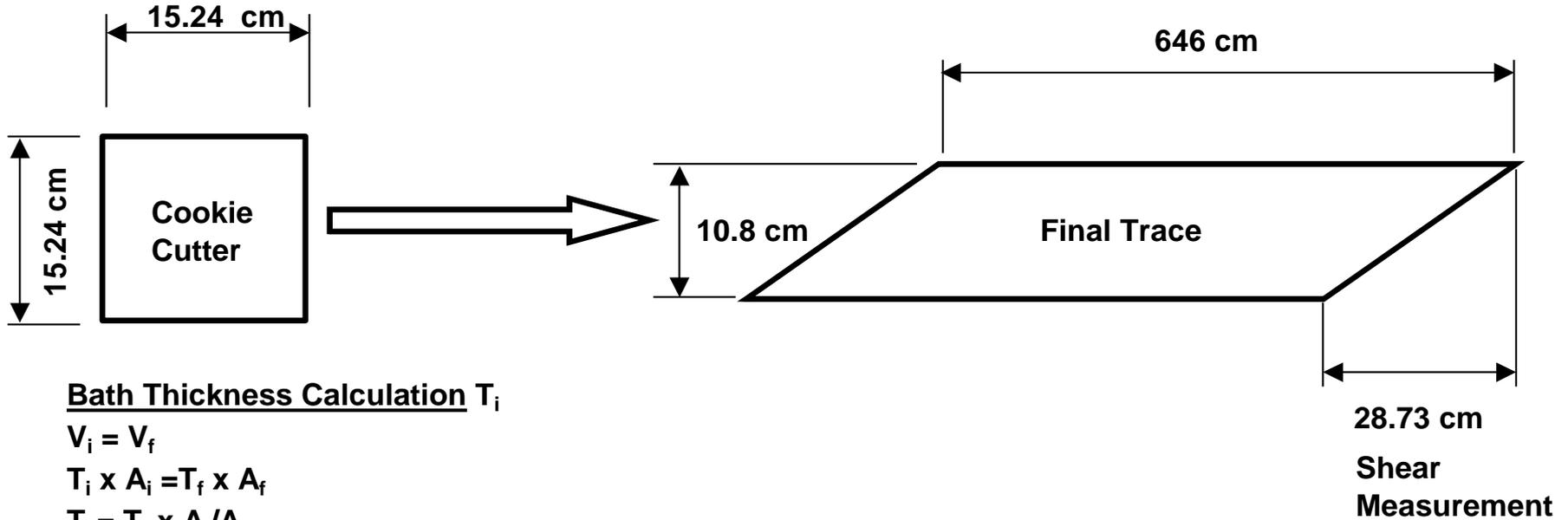


# ADS Machines

- Work in conjunction with attenuating lehr force to form ribbon thickness and width
- Impart angular force to top surface of ribbon for controlling ribbon width and speed
- Affect ribbon thickness contour
- Used for less than equilibrium thickness: ADS “Assisted Direct Stretch”
- Used for greater than equilibrium thickness: RADS “Reverse Assisted Direct Stretch”

# Cookie Cutter Sample Trace and Calculation

2.5 mm 616 TPD Bay 5-1



## Bath Thickness Calculation $T_i$

$$V_i = V_f$$

$$T_i \times A_i = T_f \times A_f$$

$$T_i = T_f \times A_f / A_i$$

$$T_i = .086 \text{ in.} \times (4 \frac{1}{4} \text{ in.} \times 25 \frac{7}{16} \text{ in.}) / 36 \text{ in.}^2$$

$$T_i = .258 \text{ in.}$$

$V_i$  = initial volume  $V_f$  = final volume

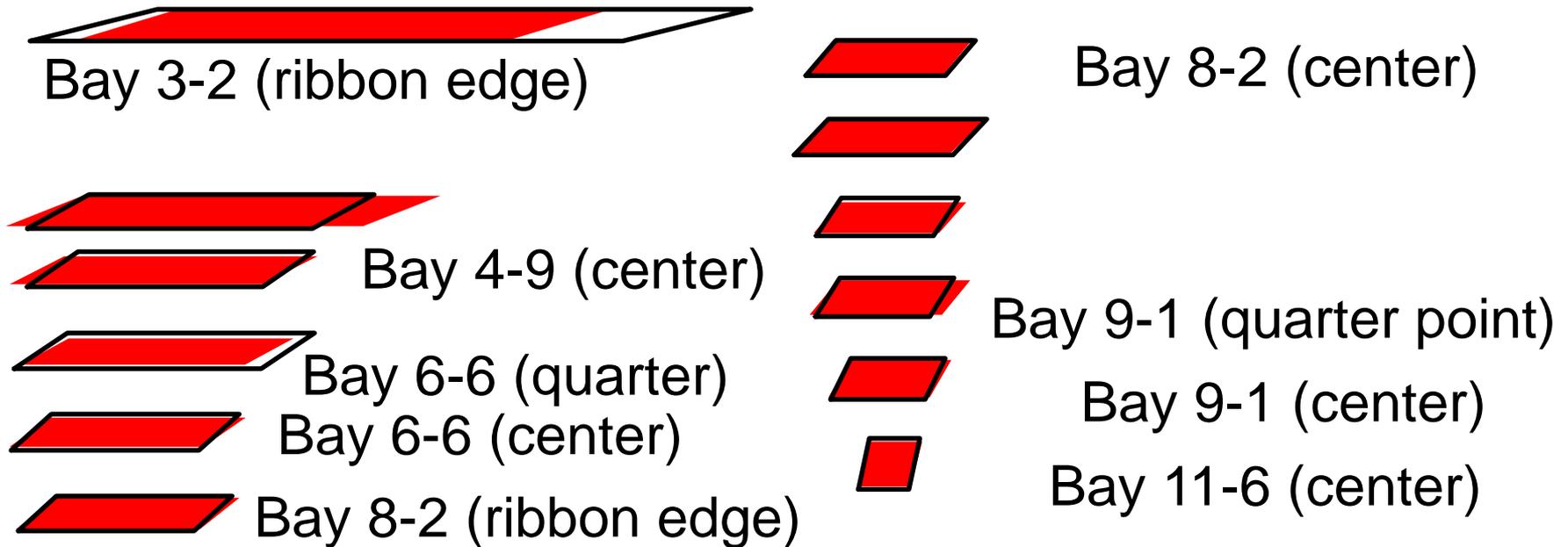
$T_i$  = initial thickness  $T_f$  = final thickness

$A_i$  = initial area  $A_f$  = final area

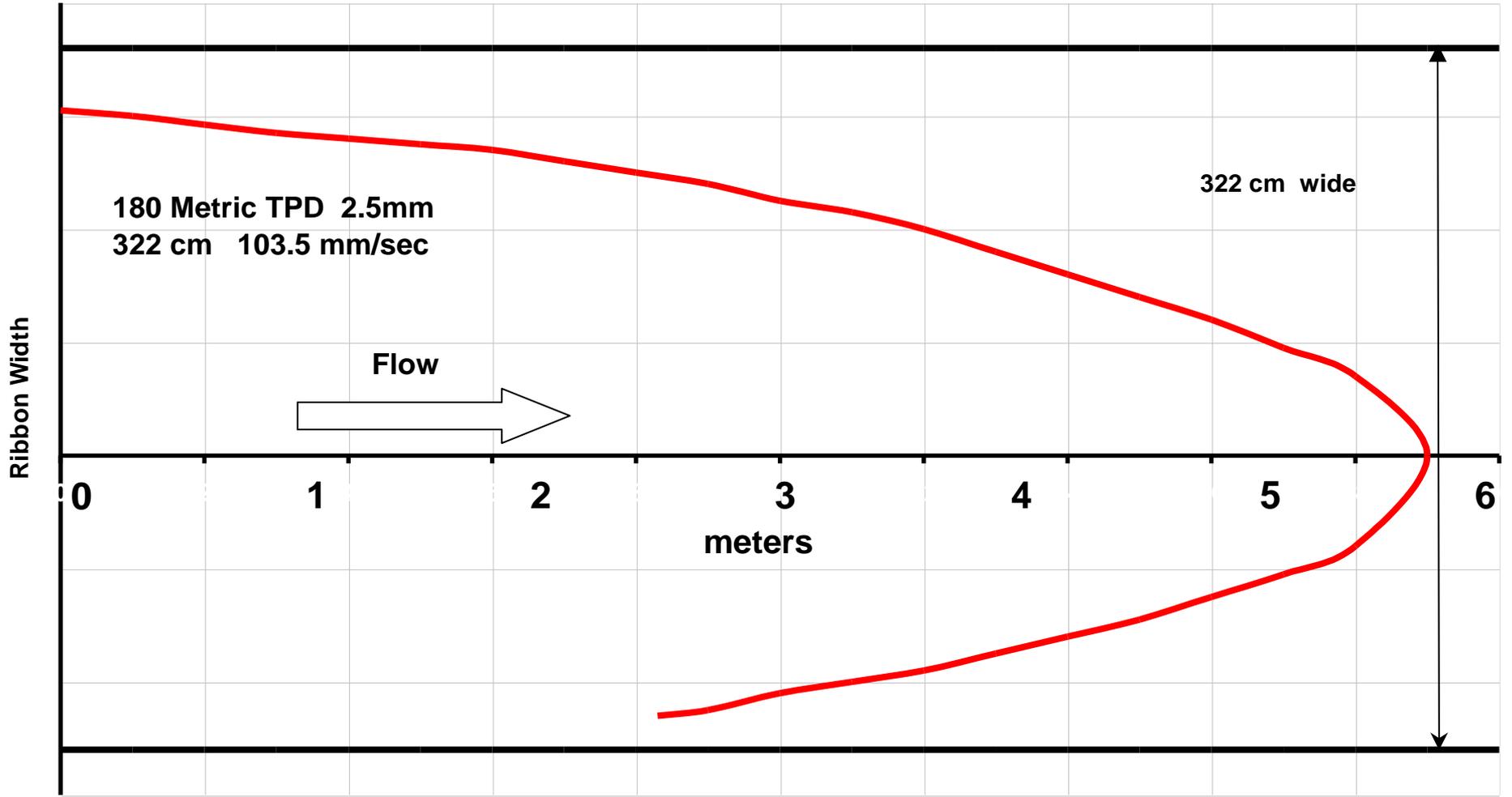
# Cookie Cutter Tests

Prediction of cookie cutter data is a very sensitive test of the model, great for model validation

□ original size     plant data    — calculated



# Sand Trace Velocity Profile



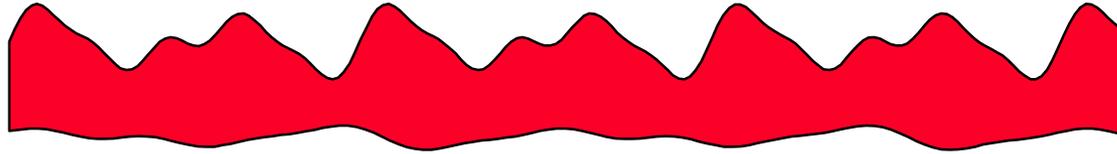
# Optical Distortion

# Float Glass: A Typical “Semi-Schlieren” Photo

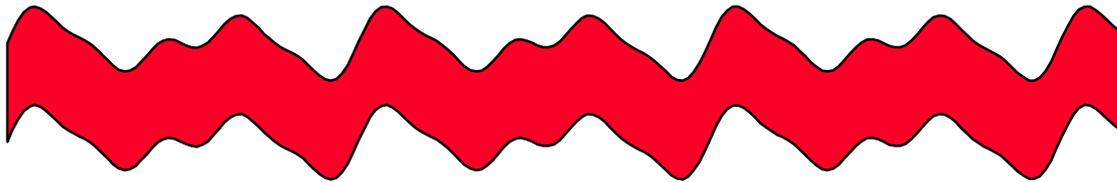
The pattern is characterized by:  
uniformity  
directionality



# Optical Distortion in Float Glass

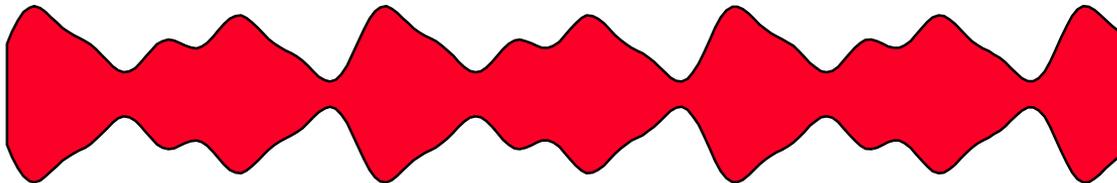


uncorrelated thickness variations

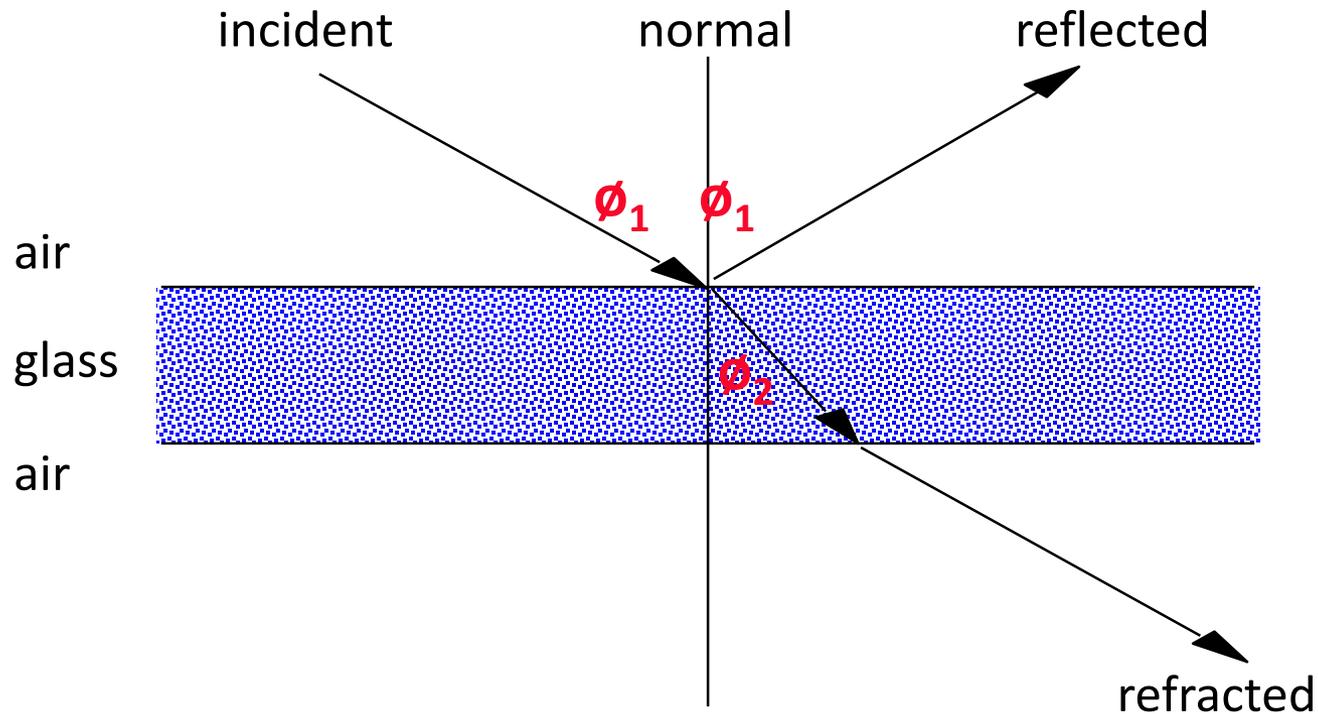


corrugations

highly anti-correlated variations ("varicose", "sausages")



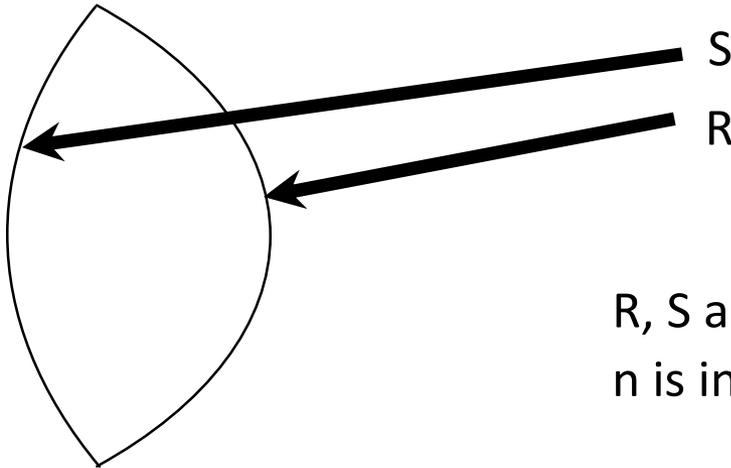
# Refraction, Snell's Law



**Snell's Law:**

$$n_1 \sin \phi_1 = n_2 \sin \phi_2$$

# Properties of Lenses



R, S are radii of curvature  
n is index of refraction

The lensmaker's equation:

$$1/f = (n - 1)(1/R + 1/S)$$

f = focal length

P = optical power (diopters)

$$P = 1/f$$

# Float Glass Quality: Qualitative Features

- Reduced distortion levels over time
- Improved internal quality
- Optical quality degrades with reduced thickness
- Optical quality degrades with increased throughput
- Product standards are generally independent of thickness

# Float Glass Manufacture

## Sources of Optical Distortion

internal quality  
poor refractories  
bath hardware/machines  
exit end



“housekeeping”, or  
passive variables

ribbon cooling  
viscous stresses  
tin flows

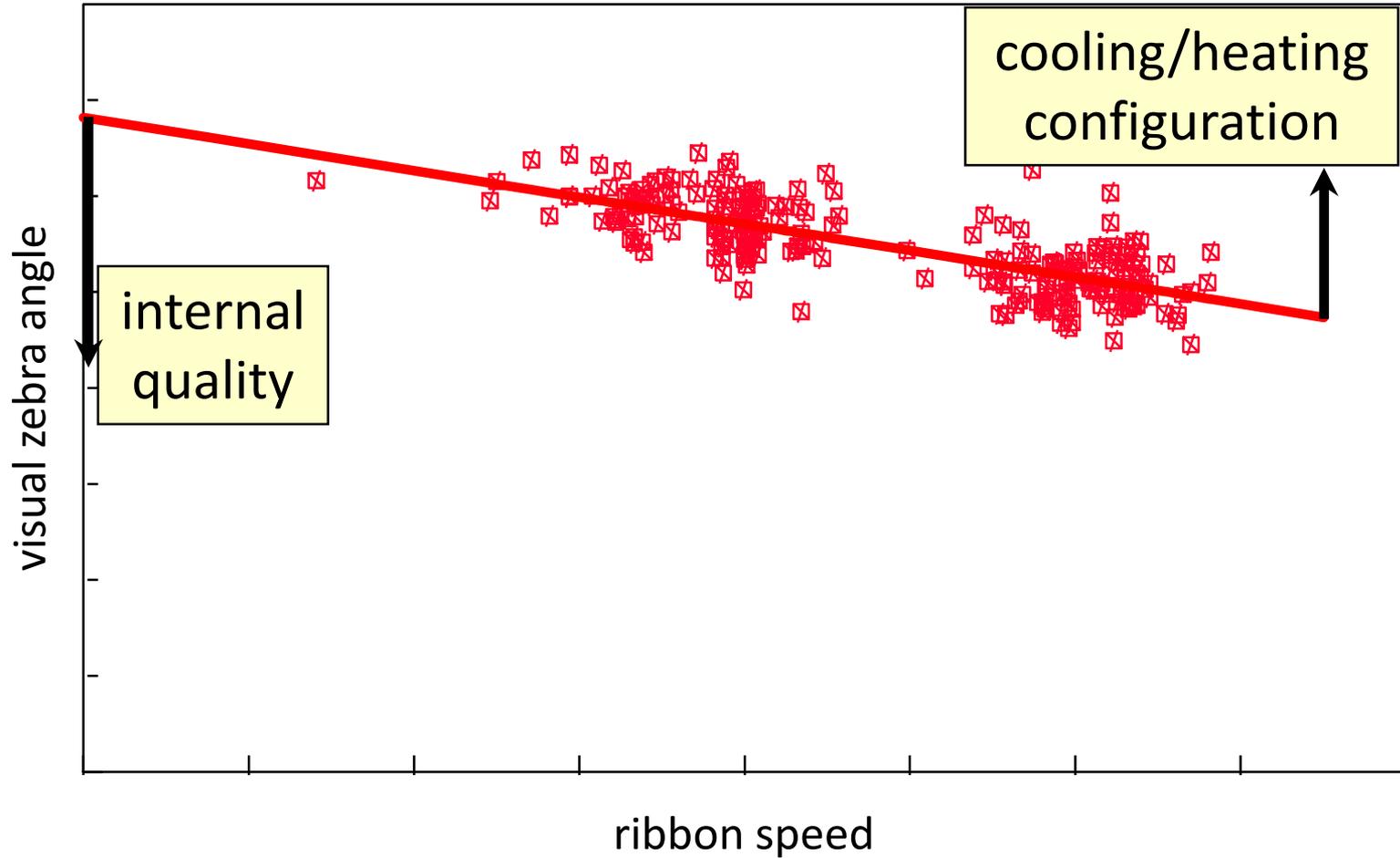


“process”, or  
active variables

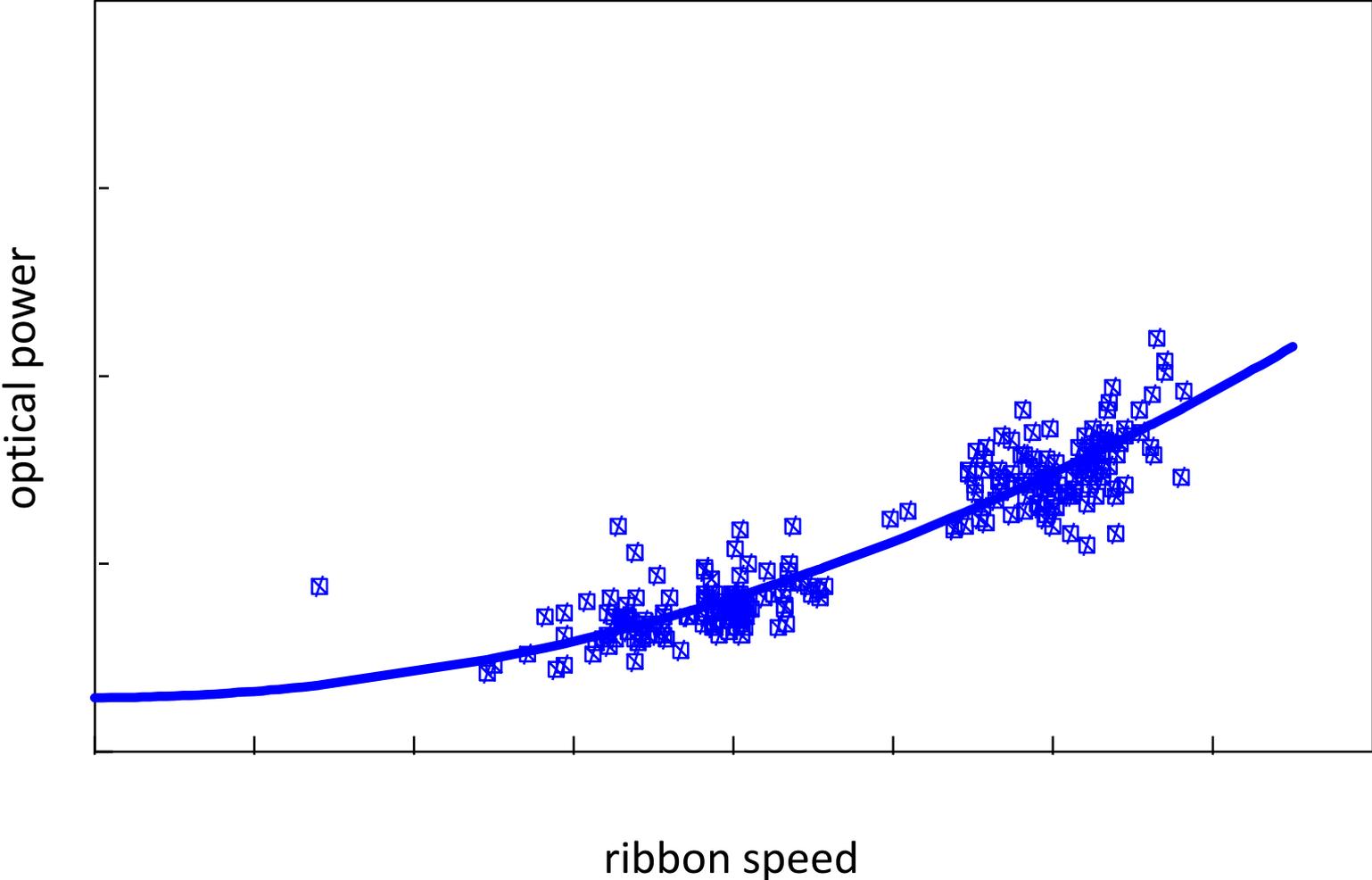
# Float Glass: Transmitted Distortion

- There are two basic sources of transmitted distortion, glass inhomogeneities and surface irregularities.
- The glass inhomogeneities originate in the furnace.
- The surface irregularities originate in the hot end of the float bath, and are caused by cooling the ribbon.
- Both have a complex bath processing component.

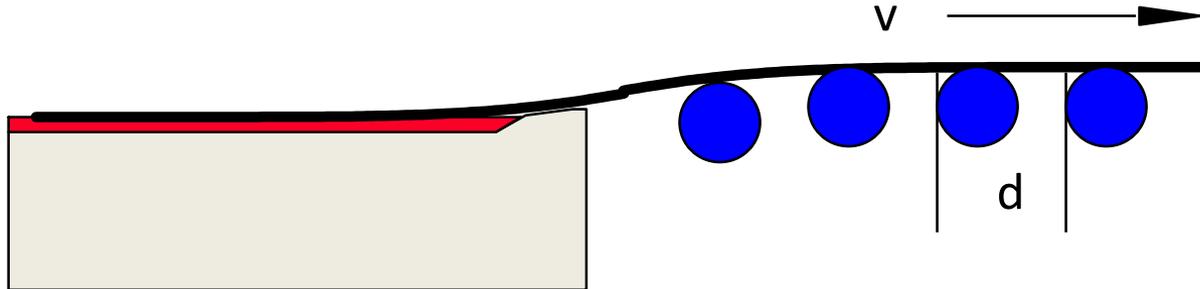
# Model Validation: Transmitted Distortion



# Model Validation: Reflected Distortion



# Modeling the Exit End



$$\begin{aligned}\text{Sag (distortion)} &= K \left( \frac{\rho g}{\mu} \right) \left( \frac{d^5}{v h^2} \right) \\ &= K \left( \frac{\rho g}{\mu} \right) \left( \frac{W d^5}{Q h} \right)\end{aligned}$$

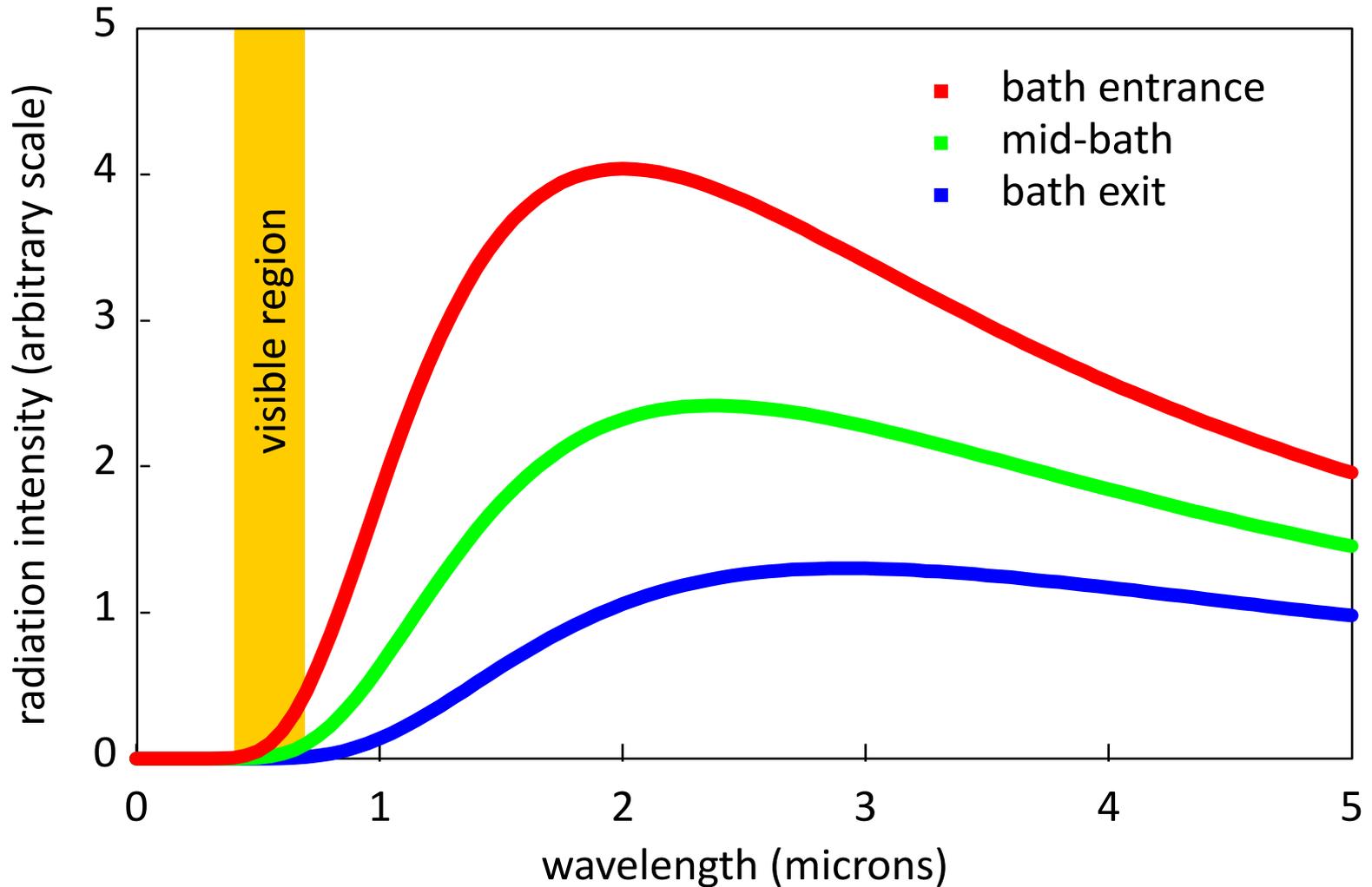
Thus, exit end distortion is inversely proportional to the ribbon viscosity and the ribbon thickness.

# Heat Transfer

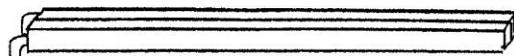
# Heat Transfer – General Comments

- Heat transfer processes in the tin bath are quite complex
- All three modes of heat transfer (radiation, convection, and conduction) are taking place simultaneously.
- Glass is diathermaneous.

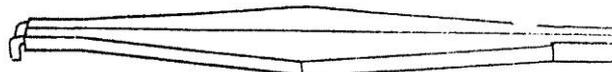
# The Planck Radiation Distribution



# Glass Ribbon Coolers

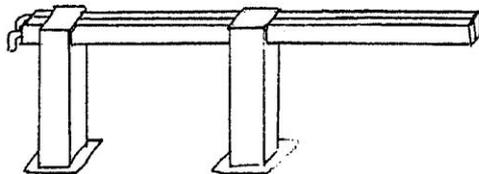


FULL RAIL

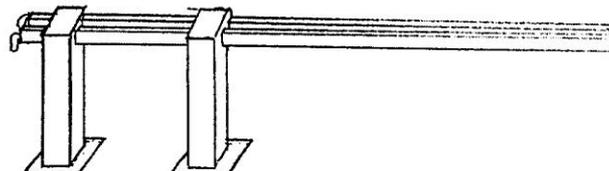


BANJO RAIL

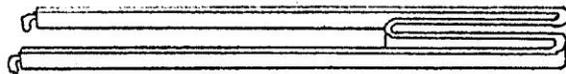
## Bath Coolers



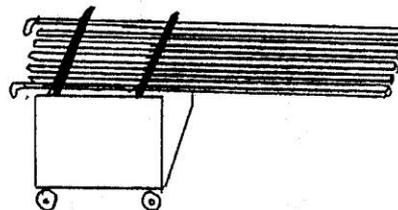
CANTILEVER RAIL  
(NON INSULATED)



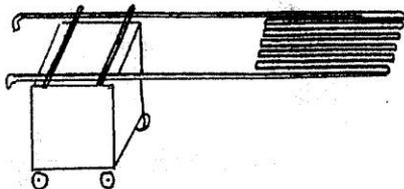
SPLIT CANTILEVER RAIL  
(NON-INSULATED)



P-COOLER  
(NON-INSULATED)



OLD STYLE C-PIPE



PREFERENTIAL C-PIPE



FULL PIPE COOLER

PPG  
Proprietary

Kapura 2/96

JD 1/03

Figure 46

# Heat Removal by Water Coolers

$$Q = MC\Delta T$$

M = amount of water (kg)

C = specific heat of water:  $\frac{1 \text{ cal}}{\text{g} \cdot ^\circ\text{C}} = \frac{1000 \text{ cal}}{\text{kg} \cdot ^\circ\text{C}}$

$\Delta T$  = temperature change of water ( $^\circ\text{C}$ )

Example: A cooler with a water flow of 378 l/min and a  $\Delta T$  of  $9^\circ\text{C}$

$$Q = (378 \text{ l/min}) \times (1 \text{ kg/l}) \times (60 \text{ min/hr}) \times (1000 \text{ cal/kg} \cdot ^\circ\text{C}) \times (9^\circ\text{C})$$

$$Q = 204,120,000 \text{ cal/hr} = 854,650 \text{ kJ/hr} \quad 1 \text{ kW} = 3600 \text{ kJ/hr}$$

$$Q = 238 \text{ kW}$$

## Shortcut

$$Q \text{ (kW)} = \text{l/min} \times \Delta T \times .07$$

$$Q = 378 \text{ l/min} \times 9 \times .07$$

$$Q = 238 \text{ (kW)}$$

# Bath Chemistry

# Metal Substrate Requirements

- Denser than glass
- Minimal chemical reactivity with glass
- Glass doesn't "wet" it
- Boiling point well above 2000 °F
- Melting point below 1100 °F
- Low vapor pressure
- Manageable metal chemistry
- Affordable

# Properties of Various Metals

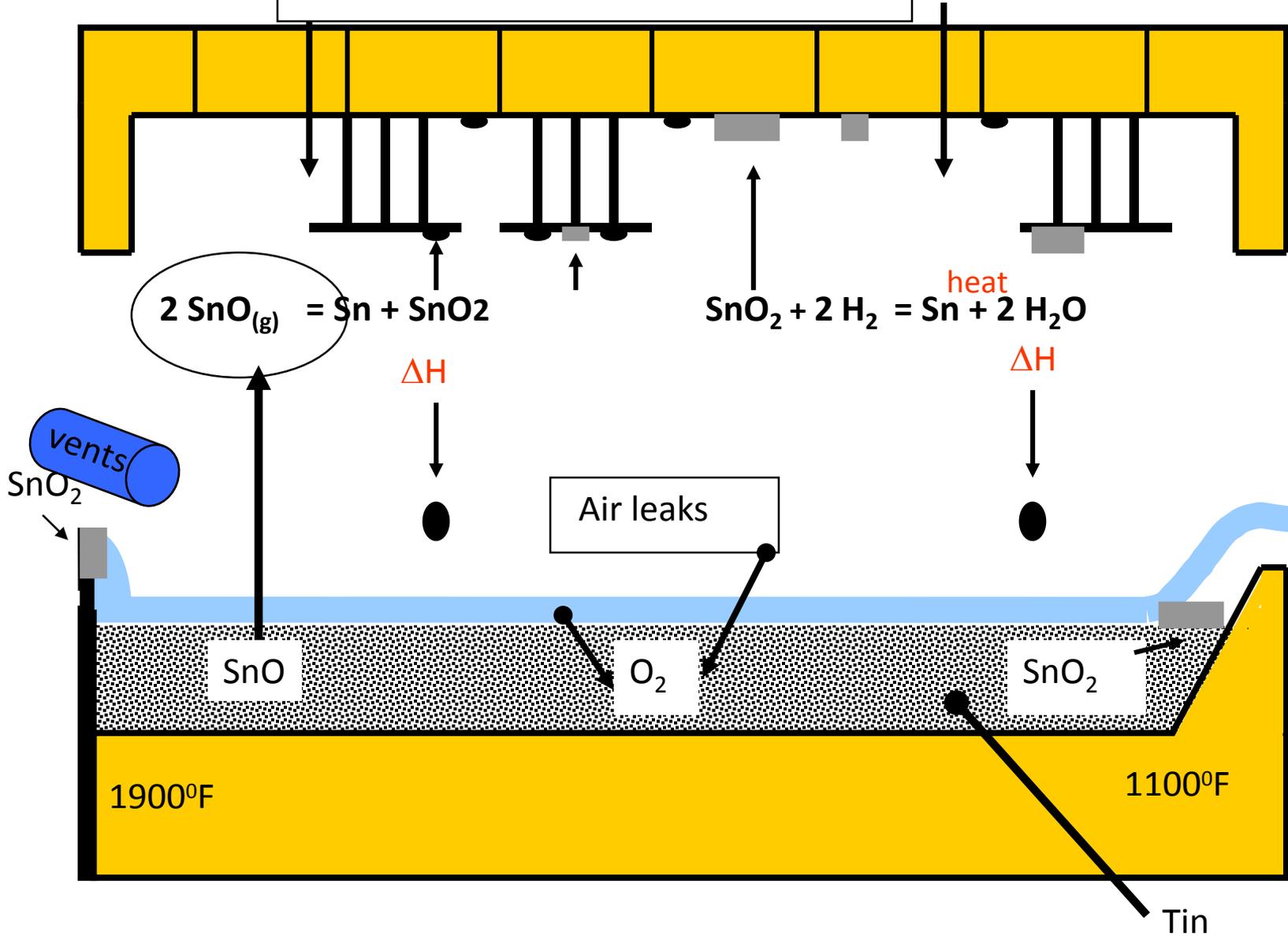
	<u>METAL</u>	<u>MELTING POINT °F</u>	<u>BOILING POINT °F</u>	<u>VAPOR PRESSURE @2000F mmHg</u>	<u>REMARKS</u>
	TIN	450	4120	.002	
INCREASING	GALLIUM	86	3600	.023	WETS GLASS
	INDIUM	313	3630	.11	
VAPOR	ALUMINUM	1220	3733	.45	WETS GLASS FORMS NITRIDE
PRESSURE	BISMUTH	520	2588	4.1	
	LEAD	621	3270	4.3	
	BARIUM	1340	2980	15	FORMS NITRIDE
	ANTIMONY	1168	2625	22	
	CALCIUM	1553	2710	32	FORMS NITRIDE
	THALLIUM	576	2637	35	
	STRONTIUM	1420	2523	82	
	CERIUM	1480	2550	-	
.....					
HIGH	GERMANIUM	1720	4900	.00003	
MELTING	SILVER	1762	3540	.027	COULD USE OXIDIZING ATM.
	GOLD	1945	4710	.00001	
POINT	COPPER	1980	4237	.0003	

# Properties of Tin

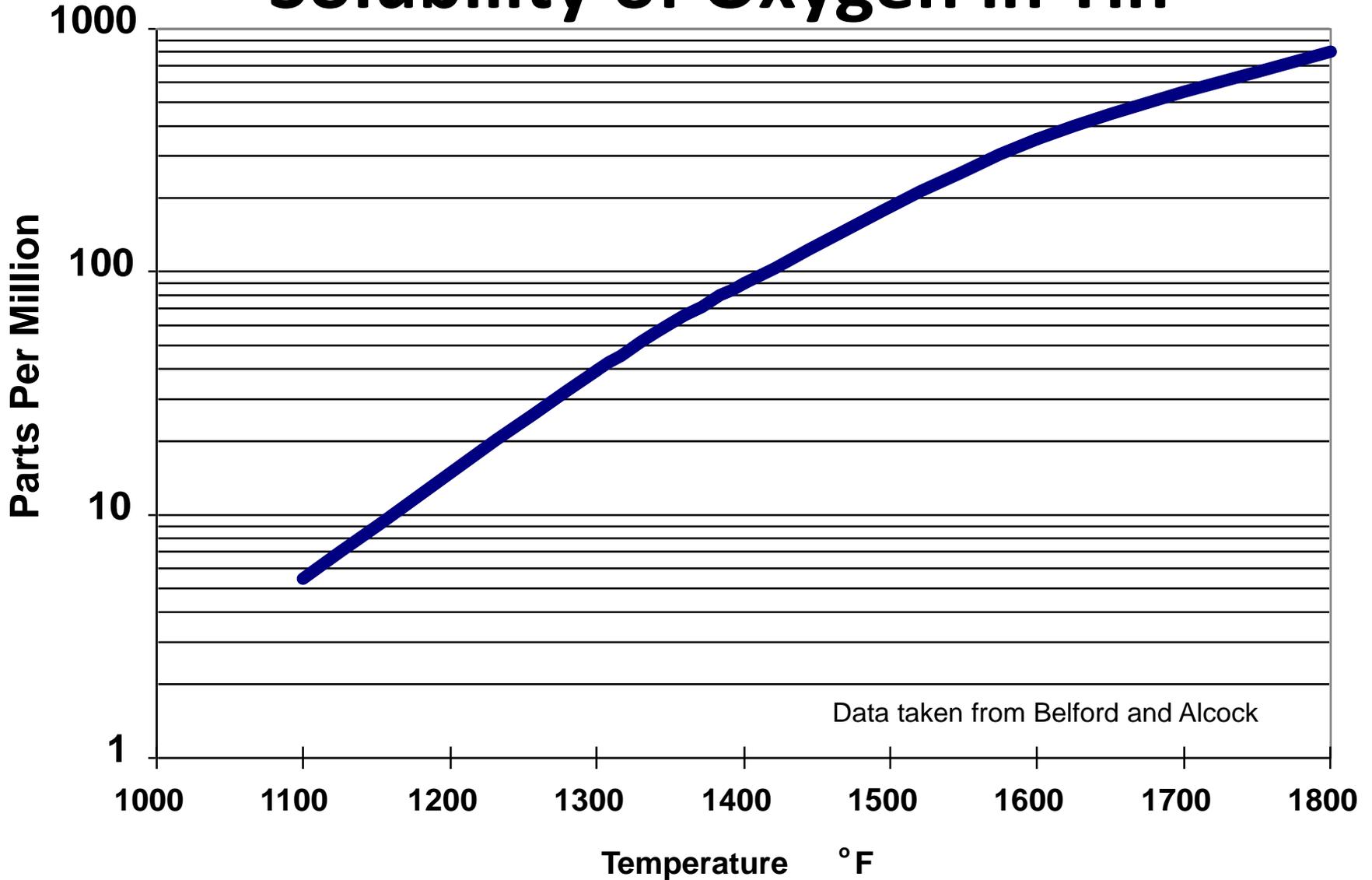
- Melting Point = 232 °C
- Boiling Point = 2271 °C
- Vapor Pressure = 0.002 mm Hg @ 1100 °C
- Density = 6.5 g/cc
- Low viscosity at bath temperatures (0.01 p)
- Low reactivity/solubility with H<sub>2</sub> and N<sub>2</sub>
- High reactivity with O<sub>2</sub>
- Does not wet the glass

# Oxygen Cycle

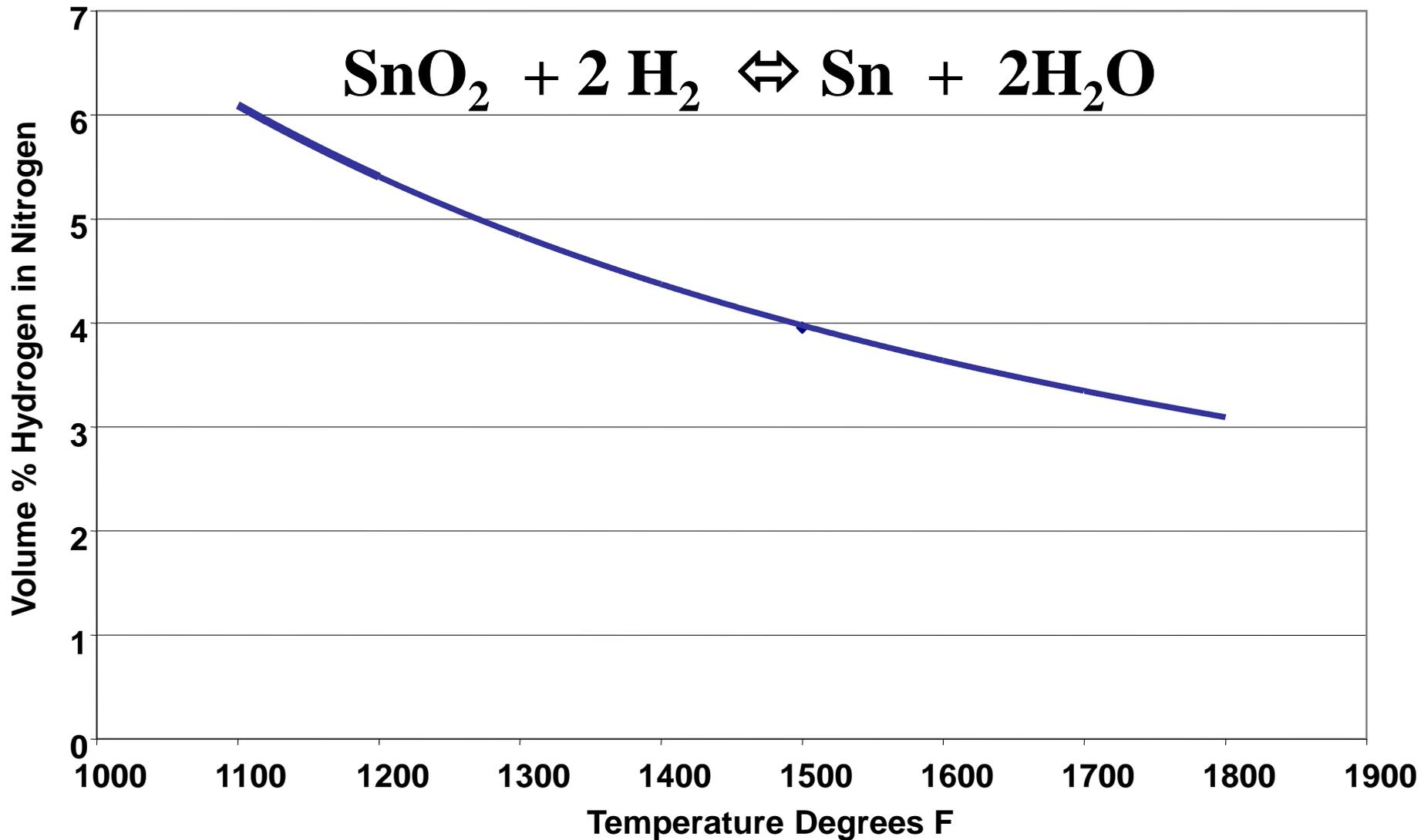
Bath Atmosphere N<sub>2</sub> + H<sub>2</sub>



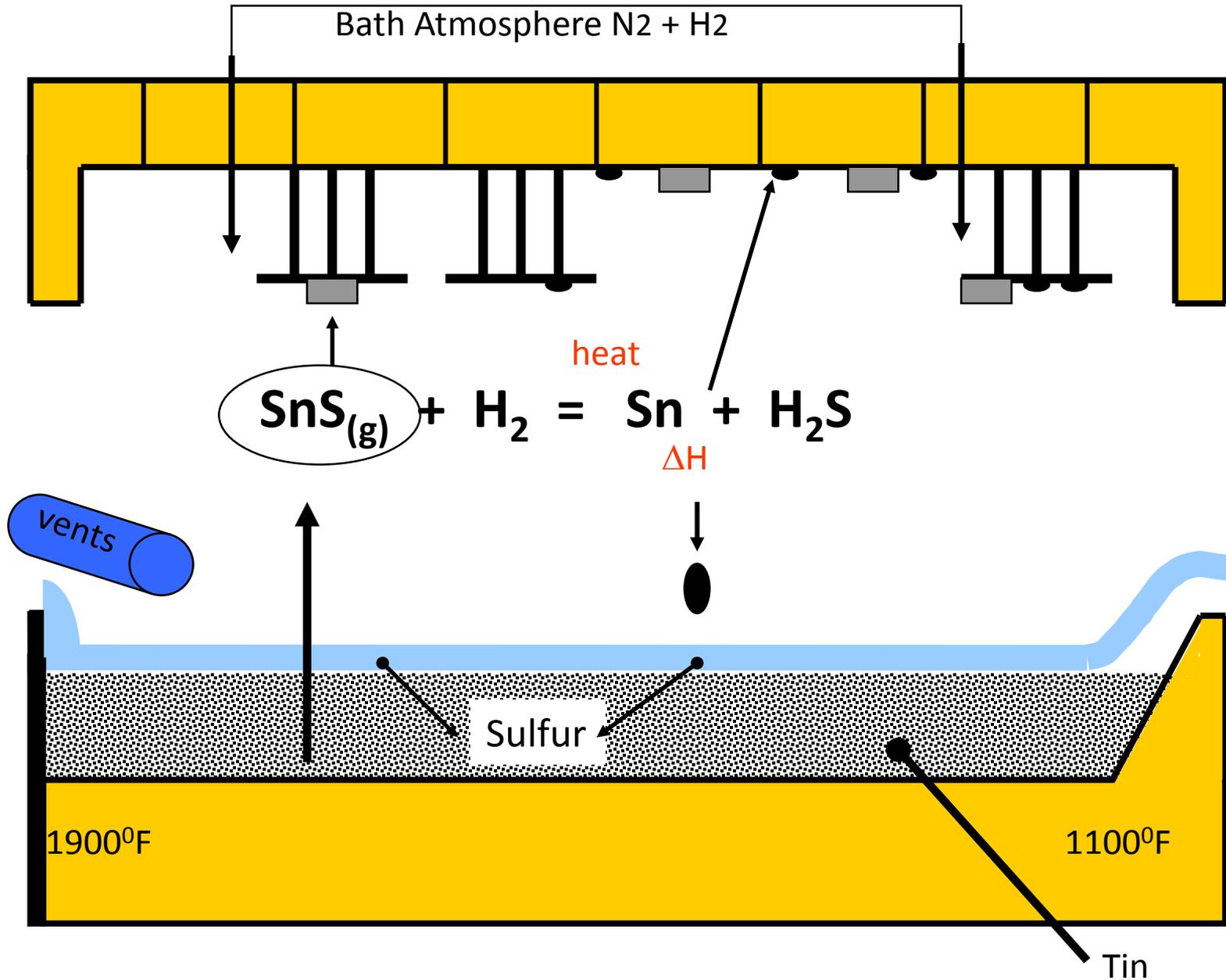
# Solubility of Oxygen in Tin



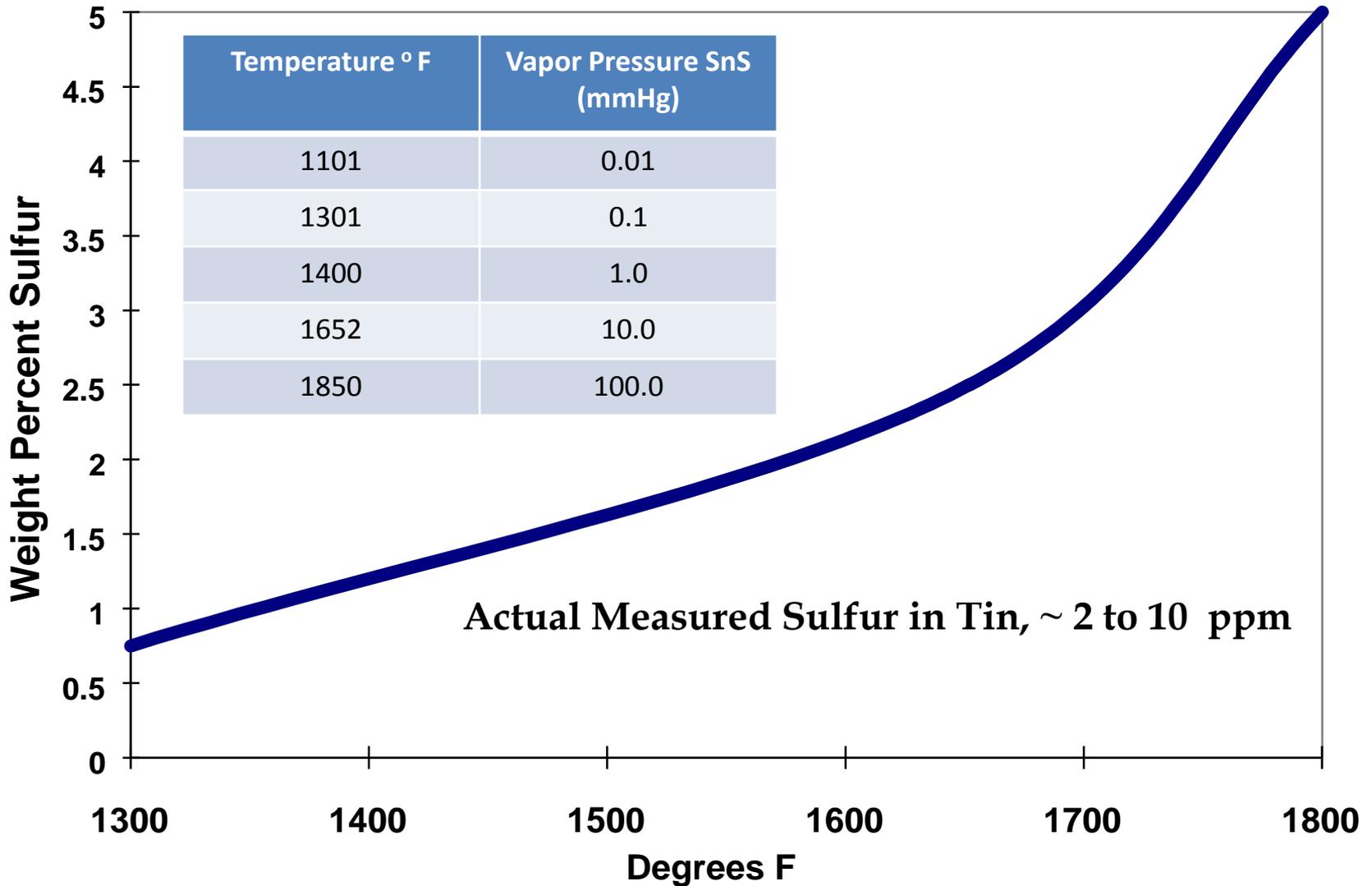
# SnO<sub>2</sub> Reduction by H<sub>2</sub>



# Sulfur Cycle



# Solubility of Sulfur in Tin



# A Bath Atmosphere Management System

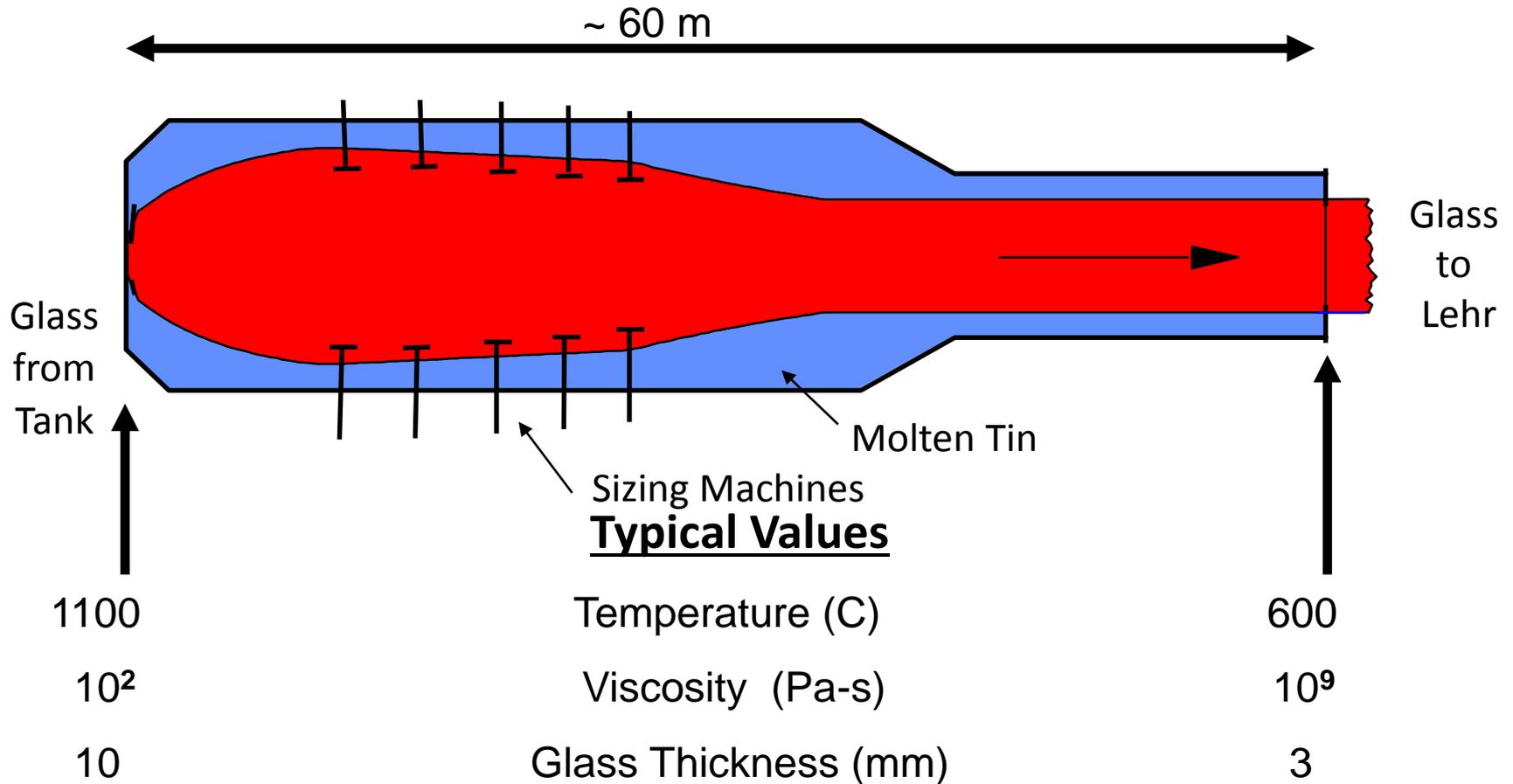
- **H<sub>2</sub> usage:** 1% - 5% throughout the bath
- **N<sub>2</sub> usage:** 50,000 – 100,000 scfh (size dependent)
- **Bath pressure:** 0.20" H<sub>2</sub>O or higher
- **Hot end venting:** vent 15-20% of the total atmosphere flow

# Bath Modeling

# Modeling Float Bath

- Three major computation fluid dynamics areas
  - Bath atmosphere flow
    - Effects bath defects like top tin
  - Glass flow
    - Need to make glass in needed thickness and width
  - Liquid tin flow
    - Influences glass temperature since tin is a liquid metal

# Plan View of A Float Glass Tin Bath



Massive glass viscosity variation  $1:10^7$

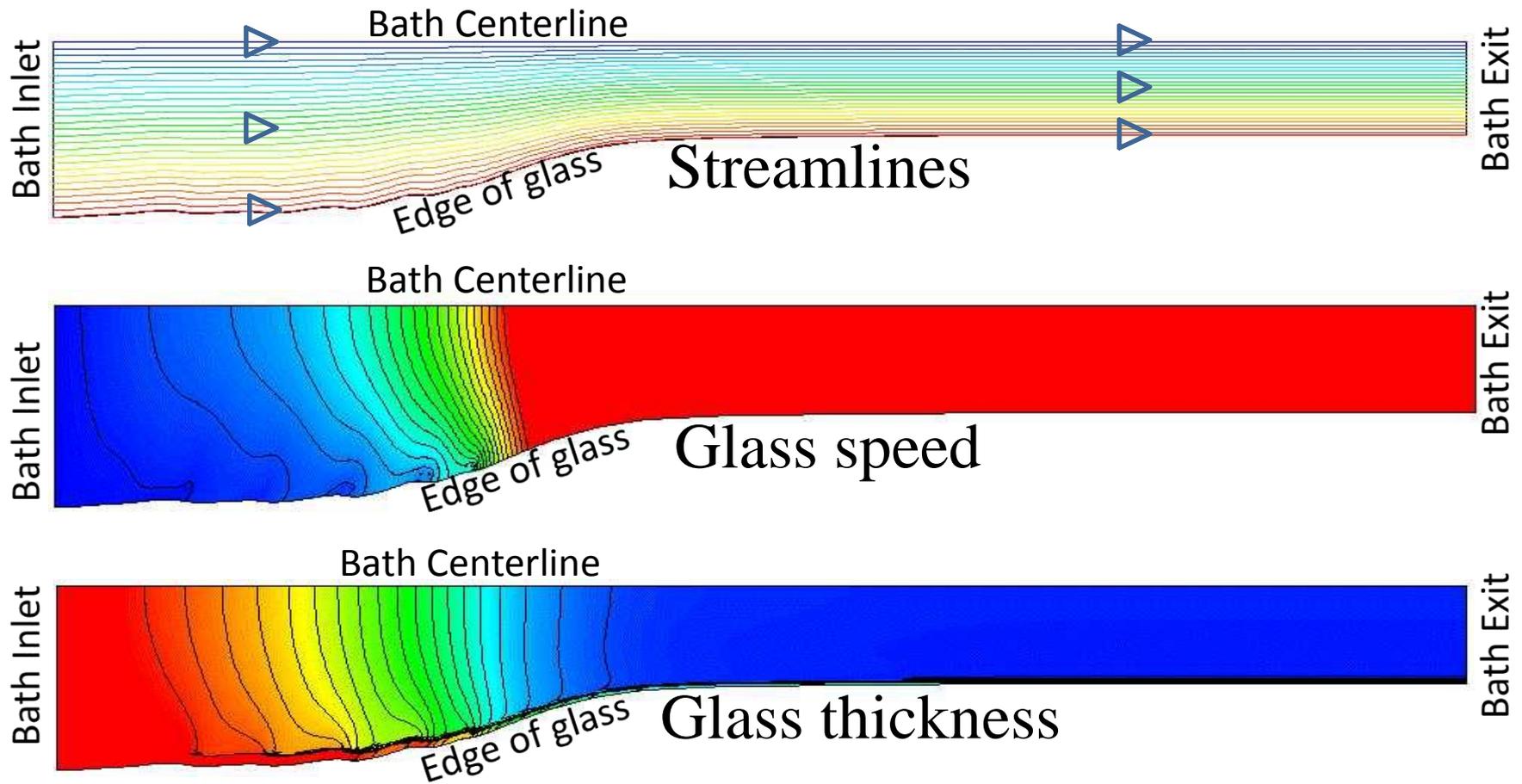
Glass aspect ratios are large - Length:Width:Thickness = 10,000:1,000:1

# Modeling Glass in Bath

- PPG has a detailed model
- Free surface model since glass thickness and width need to be calculated
- Inputs – Bath conditions (throughput, temperatures, machine speeds and angles, exit speed)
- Output
  - Glass thickness and width
  - Glass speed (residence time)
  - Glass stresses

# Model Predictions

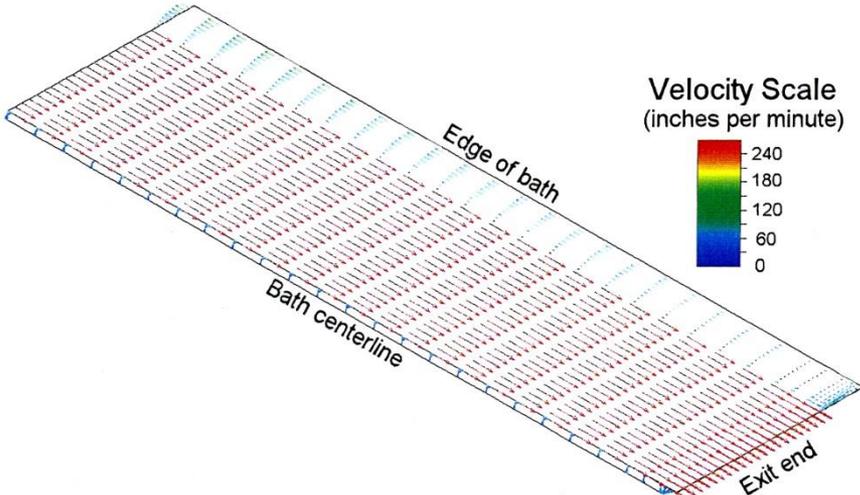
## Top View of glass in float bath



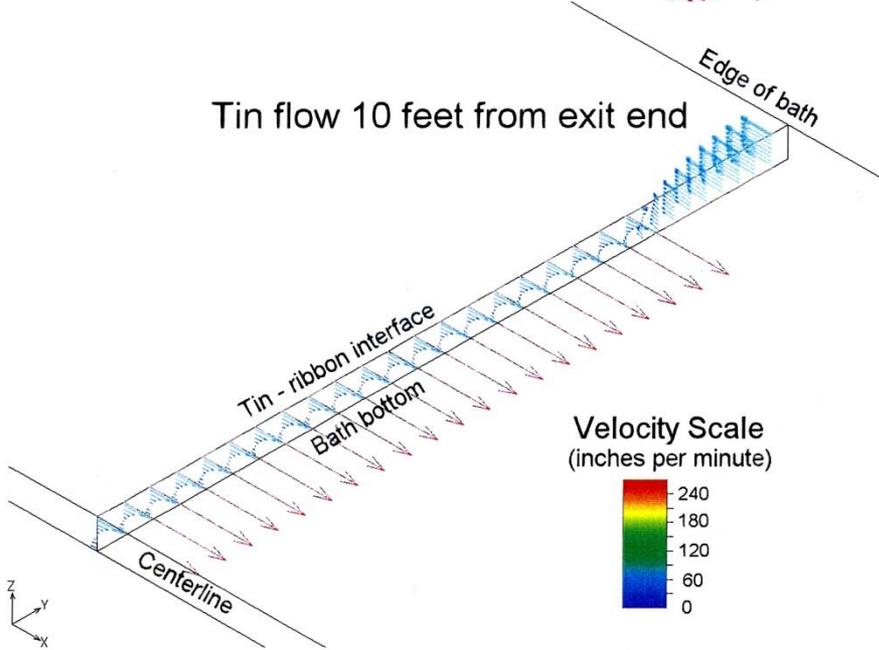
# Tin Flow Modeling

- Liquid metal flow – high thermal conductivity
- Turbulent
- Moving glass drags thin boundary layer of tin
- Return flow along the sides
- Near bath entrance tin flow may laminarize

# Typical Tin Flow Pattern at Exit End



Tin flow 10 feet from exit end



# Modeling Bath Atmosphere

- Composition generally 95% N<sub>2</sub> + 5% H<sub>2</sub>
- Turbulent gas flow
- Buoyancy effects due to bath temperatures
- Lot of variation from bath to bath since bath conditions vary

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January 25, 2015